

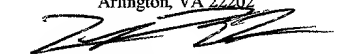
09/980168

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Atty. Dkt. No: 5333-02500

Inventor(s):
Chun Byung YangTitle: A CATALYST FOR
ETHYLENE HOMO- AND
CO-POLYMERIZATION§
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§CERTIFICATE OF EXPRESS MAIL
UNDER 37 C.F.R. §1.10"Express Mail" mailing label number: EL726368216US
DATE OF DEPOSIT: November 27, 2001

I hereby certify that this paper (along with any paper and/or fee referred to as being attached or enclosed) is being deposited with the United States Postal Service "Express Mail Post Office to Addressee" service under 37 C.F.R. § 1.10 on the date indicated above and is addressed to:

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Derrick BrownTRANSMITTAL LETTER TO THE UNITED STATES DESIGNATED/ELECTED
OFFICE (DO/EO/US) CONCERNING A FILING UNDER 35 U.S.C. § 371

INTERNATIONAL APPLICATION NO.: PCT/KR99/00639

INTERNATIONAL FILING DATE: October 23, 1999

PRIORITY DATE CLAIMED: May 27, 1999

U.S. APPLICATION NO. (If known): Unknown

Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:

1. ☒ This is a FIRST submission of items concerning a filing under 35 U.S.C. § 371.
2. ☐ This is a SECOND or SUBSEQUENT submission of items concerning a filing under 35 U.S.C. § 371.
3. ☐ This is an express request to begin national examination procedures (35 U.S.C. § 371(f)) at any time rather than delay examination until the expiration of the applicable time limit set in 35 U.S.C. § 371(b) and PCT Articles 22 and 39(I).
4. ☐ A translation of the International Application into English (35 U.S.C. § 371(c)(2)),
5. ☐ Drawings
☐ Formal Figure(s) _____ on 1 sheet(s).
6. ☒ A copy of the International Application as filed (35 U.S.C. § 371(c)(2))
☒ is transmitted herewith including: a title page; 16 page specification; 2 page(s) of claims (claims 1-5); 1 page abstract..
☐ has been transmitted by the International Bureau.
☐ is not required, as the application was filed in the United States Receiving Office (RO/US).

7. ☐ Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. § 371(c)(3))
 - ☐ are transmitted herewith (required only if not transmitted by the International Bureau).
 - ☐ have been transmitted by the International Bureau.
 - ☐ have not been made; however, the time limit for making such amendments has NOT expired.
 - ☐ have not been made and will not be made.
8. ☐ A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. § 371(c)(3)).
9. ☒ A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.
 - ☐ A copy of the Demand for International Preliminary Examination is enclosed.
10. ☐ An oath or declaration of the inventor(s) (35 U.S.C. § 371(c)(4)):
 - ☐ is enclosed (____ pages).
 - ☐ a combined Declaration and Power of Attorney is enclosed (____ pages).
 - ☒ is not enclosed. Applicant requests the Patent and Trademark Office to accept this application and accord a serial number and filing date as of the date this application is deposited with the U.S. Postal Service for Express Mail. Further, Applicant requests that the NOTICE OF MISSING PARTS-FILING DATE GRANTED be sent to the undersigned representative of Applicant.
11. ☒ Applicant hereby claims priority to:
 - ☒ International Application No.: PCT/KR99/00639 filed October 23, 1999.
 - ☒ Korean application No.: KR 1999/19192 filed May 27, 1999.
12. ☐ A translation of the annexes of the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. § 371(c)(5)).
13. ☒ The entire disclosure of the International Application referred to above is considered to be part of the accompanying application and is hereby incorporated by reference herein.
14. ☐ Assignment Papers.
 - ☐ An assignment document is enclosed for recording (____ pages).
 - ☐ Form PTO-1595 Assignment Recordation Cover Sheet (____ page).
15. ☒ A Preliminary Amendment (7 pages).
16. ☒ A substitute specification for pages 1-14, 17 (17 pages).
17. ☒ A strikethrough version of specification and abstract (18 pages).
18. ☐ Power of Attorney
 - ☐ Is enclosed.
 - ☐ a combined Declaration and Power of Attorney is enclosed.
19. ☐ Information Disclosure Statement (IDS), including:
 - ☐ Form PTO-1449
 - ☐ Reference(s) marked according to Form PTO-1449.
20. ☒ Return Receipt Postcard
21. ☐ Small Entity Status
 - ☐ A small entity statement is enclosed.
22. ☐ Copy of PCT Form PCT/IB/338
23. ☐ Copy of International Request.

09/980168

24. ☒ Copy of International Preliminary Examination Report.
☐ A copy of the International Preliminary Examination Report in French.
☐ English Translation of the International Preliminary Examination Report.

25. ☒ The following fees are submitted:

BASIC NATIONAL FEE (37 CFR § 1.492 (a) (1)-(5):				
<input type="checkbox"/> Neither international preliminary examination fee nor international search fee paid to USPTO and International Search Report not prepared by the EPO or JPO.....				\$970.00
<input checked="" type="checkbox"/> International preliminary examination fee not paid to USPTO but International Search Report prepared by the EPO or JPO.....				\$890.00
<input type="checkbox"/> International preliminary examination fee not paid to USPTO but international search fee paid to USPTO.....				\$760.00
<input type="checkbox"/> International preliminary examination fee paid to USPTO but all claims did not satisfy provisions of PCT Article 33(1)-(4).....				\$670.00
<input type="checkbox"/> International preliminary examination fee paid to USPTO and all claims satisfied provisions of PCT Article 33(1)-(4).....				\$96.00
ENTER APPROPRIATE BASIC NATIONAL FEE AMOUNT (as selected above):				\$890.00
Surcharge of \$130.00 for furnishing oath or declaration later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 Months from the earliest claimed priority date (37 C.F.R. § 1.492(e)).				
CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE	
Total claims	26 - 20 =	6	6 x \$18.00 =	108.00
Independent claims	3 - 3 =	0	x \$78.00 =	
MULTIPLE DEPENDENT CLAIM(S)			+ \$260.00 =	
TOTAL OF ABOVE CALCULATIONS:				\$998.00
Reduction by 50% for Small Entity. A Small Entity Statement must be filed:				
SUBTOTAL:				\$998.00
Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 Months from the earliest claimed priority date:				
TOTAL NATIONAL FEE:				
Fee for recording the enclosed assignment. The assignment must be accompanied by an appropriate cover sheet. \$40.00 per property:				
TOTAL FEES ENCLOSED:				\$998.00

☒ A fee authorization in the amount of \$998.00 is enclosed.

☐ Please charge my Deposit Account No. 50-1505/ in the amount of to cover the above fees.

☒ The Commissioner is hereby authorized to charge any other fees which may be required or credit any overpayment to Conley, Rose, & Tayon, P.C., Deposit Account No. 50-1505/5333-02500/EBM.

JC10 Rec'd PGT/PTO 27 NOV 2001

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[illegible]

JC10 Rec'd PCT/PTO 27 NOV 2001

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

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Derrick Brown

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*In the Claims:*

Please cancel claims 1-5 without prejudice.

Please add the following claims.

6. (new) A solid titanium catalyst for homo-polymerization and co-polymerization of ethylene, wherein the catalyst is produced by:

preparing a magnesium compound solution by contacting a magnesium halide compound with an alcohol;

preparing a second solution by reacting the magnesium compound solution with an ester compound and a first silicon compound; and

reacting the second solution with a mixture of a titanium compound and a second silicon compound to produce the solid titanium catalyst.

7. (new) The solid titanium catalyst of claim 6, wherein the produced solid titanium catalyst is further reacted with a second titanium compound.

8. (new) The solid titanium catalyst of claim 6, wherein the ester compound comprises an ester compound having at least one hydroxy group.

9. (new) The solid titanium catalyst of claim 6, wherein the ester compound comprises an unsaturated aliphatic ester having at least one hydroxy group.

10. (new) The solid titanium catalyst of claim 6, wherein the ester compound comprises 2-

hydroxy ethylacrylate, 2-hydroxy ethylmethacrylate, 2-hydroxy propyl acrylate, 2-hydroxy propylmethacrylate, 4-hydroxy butylacrylate, or pentaerithritol triacrylate.

11. (new) The solid titanium catalyst of claim 6, wherein the ester compound comprises an aliphatic monoester having at least one hydroxy group or an aliphatic polyester having at least one hydroxy group.

12. (new) The solid titanium catalyst of claim 6, wherein the ester compound comprises 2-hydroxy ethyl acetate, methyl 3-hydroxy butylate, ethyl 3-hydroxy butylate, methyl 2-hydroxy isobutylate, ethyl 2-hydroxy isobutylate, methyl 3-hydroxy-2-methyl propionate, 2,2-dimethyl-3-hydroxy propionate, ethyl-6-hydroxy hexanoate, t-butyl-2-hydroxy isobutylate, diethyl-3-hydroxy glutarate, ethyllactate, isopropyl lactate, butyl-isobutyl lactate, isobutyl lactate, ethyl mandelate, dimethyl ethyl tartrate, ethyl tartrate, dibutyl tartrate, diethyl citrate, triethyl citrate, ethyl-2-hydroxy-caproate, or diethyl *bis*-(hydroxymethyl) malonate.

13. (new) The solid titanium catalyst of claim 6, wherein the ester compound comprises an aromatic ester having at least one hydroxy group.

14. (new) The solid titanium catalyst of claim 6, wherein the ester compound comprises 2-hydroxy ethyl benzoate, 2-hydroxy ethyl salicylate, methyl-4-(hydroxy methyl) benzoate, methyl-4-hydroxy benzoate, ethyl-3-hydroxy benzoate, 4-methyl salicylate, ethyl salicylate, phenyl salicylate, propyl-4-hydroxy benzoate, phenyl-3-hydroxy naphthanoate, monoethylene glycol monobenzoate, diethylene glycol benzoate, or triethylene glycol monobenzoate.

15. (new) The solid titanium catalyst of claim 6, wherein the ester compound comprises an alicyclic ester having at least one hydroxy group.

16. (new) The solid titanium catalyst of claim 6, wherein the first silicon compound comprises a

silicon compound having an alkoxy group.

17. (new) The solid titanium catalyst of claim 6, wherein the first silicon compound comprises the general formula  $R^1_nSi(OR^2)_{4-n}$ , wherein  $R^1$  comprises a hydrocarbon having between 1 to 12 carbons, wherein  $R^2$  comprises a hydrocarbon having between 1 to 12 carbons, and wherein  $n$  comprises an integer between 0 and 3.

18. (new) The solid titanium catalyst of claim 6, wherein the first silicon compound comprises dimethyldimethoxy silane, dimethyldiethoxy silane, diphenyldimethoxy silane, methylphenyldimethoxy silane, diphenyldiethoxy silane, ethyltrimethoxy silane, vinyltrimethoxy silane, methyltrimethoxy silane, phenyltrimethoxy silane, methyltriethoxy silane, ethyltriethoxy silane, vinyltriethoxy silane, butyltriethoxy silane, phenyltriethoxy silane, ethyltriisopropoxy silane, vinyltributoxy silane, ethylsilicate, butylsilicate, or methyltriaryloxy silane.

19. (new) The solid titanium catalyst of claim 6, wherein the titanium compound comprises the general formula  $Ti(OR)_aX_{4-a}$ , wherein  $R$  comprises an alkyl group with 1 to 20 carbon atoms, wherein  $X$  comprises a halogen atom, and wherein  $a$  comprises an integer between 0 and 4.

20. (new) The solid titanium catalyst of claim 6, wherein the titanium compound comprises a titanium tetrahalide, wherein the titanium tetrahalide comprises  $TiCl_4$ ,  $TiBr_4$ , or  $TiI_4$ .

21. (new) The solid titanium catalyst of claim 6, wherein the titanium compound comprises an alkoxy-titanium trihalide, wherein the alkoxy-titanium trihalide comprises  $Ti(OCH_3)Cl_3$ ,  $Ti(OC_2H_5)Cl_3$ ,  $Ti(OC_2H_5)Br_3$ , or  $Ti(O(i-C_4H_9))Br_3$ .

22. (new) The solid titanium catalyst of claim 6, wherein the titanium compound comprises an alkoxy-titanium dihalide, wherein the alkoxy-titanium dihalide comprises  $Ti(OCH_3)_2Cl_2$ ,  $Ti(OC_2H_5)_2Cl_2$ ,  $Ti(OC_2H_5)_2Br_2$ , or  $Ti(O(i-C_4H_9))_2Cl_2$ .

23. (new) The solid titanium catalyst of claim 6, wherein the titanium compound comprises a tetraalkoxy-titanium compound, wherein the tetraalkoxy-titanium compound comprises  $\text{Ti}(\text{OCH}_3)_4$ ,  $\text{Ti}(\text{OC}_2\text{H}_5)_4$ , or  $\text{Ti}(\text{OC}_4\text{H}_9)_4$ .

24. (new) The solid titanium catalyst of claim 6, wherein the second silicon compound comprises the general formula  $\text{R}_n\text{SiCl}_{4-n}$ , wherein R comprises hydrogen, or R comprises an alkyl group, an alkoxy group, a haloalkyl group, or an aryl group having 1 to 10 carbon atoms, or R comprises a halosilyl group or a halosilyl alkyl group having 1 to 8 carbon atoms, and wherein n comprises an integer between 0 and 4.

25. (new) The solid titanium catalyst of claim 6, wherein the second silicon compound comprises silicon tetrachloride.

26. (new) The solid titanium catalyst of claim 6, wherein the second silicon compound comprises a trichlorosilane, wherein the trichlorosilane comprises methyltrichlorosilane, ethyltrichlorosilane, or phenyl-trichlorosilane.

27. (new) The solid titanium catalyst of claim 6, wherein the second silicon compound comprises a dichlorosilane, wherein the dichlorosilane comprises dimethyldichlorosilane, diethyldichlorosilane, diphenyldichlorosilane, or methylphenyldichlorosilane.

28. (new) The solid titanium catalyst of claim 6, wherein the second silicon compound comprises trimethylchlorosilane.

29. (new) The solid titanium catalyst of claim 6, wherein the ester compound comprises 2-hydroxyethyl methacrylate, wherein the first silicon compound comprises silicon tetraethoxide, wherein the titanium compound comprises titanium tetrachloride, and wherein the second silicon

compound comprises silicon tetrachloride.

30. (new) A method for producing a solid titanium catalyst, comprising:

preparing a magnesium compound solution by contacting a magnesium halide compound with an alcohol;

preparing a second solution by reacting the magnesium compound solution with an ester compound and a first silicon compound; and

reacting the second solution with a mixture of a titanium compound and a second silicon compound to produce the solid titanium catalyst.

31. (new) A solid titanium catalyst for homo-polymerization and co-polymerization of ethylene, wherein the catalyst is produced by:

preparing a magnesium compound solution by contacting a magnesium halide compound with an alcohol;

preparing a second solution by reacting the magnesium compound solution with an ester compound having at least one hydroxy group and a first silicon compound having an alkoxy group; and

reacting the second solution with a mixture of a titanium compound and a second silicon compound to produce the solid titanium catalyst.

***In the Abstract:***

Please replace the abstract with the enclosed substitute sheet. Applicant has also submitted herewith a strikethrough version of the abstract indicating the amendments.

It is believed that no fees are due in connection with the filing of this Preliminary Amendment. However, if any fees are due, the Assistant Commissioner is hereby authorized to deduct said fees from Conley, Rose & Tayon Deposit Account No. 50-1505/5333-02500/EBM.

Respectfully submitted,



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Date: 11/27/01

## BACKGROUND OF THE INVENTION

### 1. FIELD OF THE INVENTION

The present invention relates to a catalyst for homo-polymerization or co-polymerization of ethylene, or more particularly to a high-activity titanium solid complex catalyst supported in a carrier containing magnesium, the catalyst showing high catalytic activity, high bulk density, and high hydrogen sensitivity.

### 2. DESCRIPTION OF THE RELATED ART

Catalysts containing magnesium for polymerization or co-polymerization of ethylene are known to have very high catalytic activities and to accord good bulk density, which are in turn suitable for liquid phase or gas phase polymerization. By liquid phase polymerization of ethylene, it denotes the polymerization process performed in such medium of bulk ethylene, isopentane, or hexane, and as for the important characteristics in consideration of the applicability of the catalyst used in this process, they are as follows: high activity, bulk density, the amount of molecules of low molecular weight dissolved in a medium, etc. Furthermore, in most of these manufacturing processes, hydrogen is used to control the molecular weight. The changes in the molecular weight (hereinafter hydrogen sensitivity) according to the amount of hydrogen is another characteristic of a catalyst, which is different per catalyst. The catalyst with high hydrogen sensitivity can control the molecular weight by using less amount of hydrogen at the time of the application of the process. As such, it provides more leeway with respect to the operation of the process.

Many of the titanium-based catalysts containing magnesium for olefin polymerization, and the manufacturing methods thereof have been reported. Especially, many processes making use of magnesium solutions to obtain olefin polymerization catalysts of good bulk density have been known. There is a means of obtaining a magnesium solution by reacting magnesium compounds with such electron donors as alcohol, amine, cyclic ether, or organic carboxylic acid in the presence of a hydrocarbon solvent. As for the cases of use of alcohol, they are disclosed in US Patent Nos. 4,330,649, and 5,106,807. Further, the methods for production of catalysts

containing magnesium by reacting a liquid magnesium solution with a halide compound such as titanium tetrachloride are well known. Such catalysts provide good bulk density, but there is much yet to be improved with respect to their catalytic activities and hydrogen sensitivity. In US Patent Nos. 4,477,639 and 4,518,706, a cyclic ether, tetrahydrofuran was used as a solvent of the magnesium compound.

US Patent Nos. 4,847,227, 4,816,433, 4,829,037, 4,970,186, and 5,130,284 claimed the methods of producing olefin polymerization catalysts of good bulk density, with superior polymerization activity due to the reaction of a titanium chloride compound with an electron donor compound such as magnesium alkoxide, dialkyl phthalate, and phthaloyl chloride.

US Patent No. 5,459,116 reports the method of producing supported titanium solid catalysts by means of contact-reacting a titanium compound and a magnesium solution containing an ester having at least one hydroxy group as an electron donor. By using this method, it is possible to obtain a catalyst of superior polymerization activity and bulk density. However, there remain things to be improved with respect to hydrogen sensitivity.

US Patent No. 5,869,418 shows the method of increasing hydrogen sensitivity by using a dialkoxyphenylalkane in the propylene polymerization as an external electron donor, and the advantages of such method. However, the above effects were obtained by using the external electron donor in addition to the solid catalyst, and also it is limited to polymerization and copolymerization of propylene.

### SUMMARY OF THE INVENTION

As shown above, there is a need for the development of a new catalyst for homopolymerization or copolymerization of ethylene for producing polymers with the following conditions: simple manufacturing process, high polymerization activity, high bulk density for polymers by means of controlling the catalyst particles, and high hydrogen sensitivity. In the present invention, therefore, it is intended to provide a method for producing, from low-cost compounds via a simple process, a catalyst having an excellent catalytic activity, and superior hydrogen sensitivity, capable of producing polymers of good bulk density. Further, the specific

production process of catalysts and the steps thereof as disclosed in the present invention have never been reported in the prior art.

Consequently, the objective of the present invention is to provide a new catalyst solid component for homo-polymerization or co-polymerization of ethylene, said catalyst having superior catalytic activity and hydrogen sensitivity, capable of producing polymers of high bulk density. More specifically, the objective of the present invention lies in providing a catalyst solid component for homo-polymerization or co-polymerization of ethylene, having a superior hydrogen sensitivity, wherein the form of the catalyst particles are controlled therein.

Another objective of the present invention is to provide a simple process for producing a catalyst for homo-polymerization or co-polymerization of ethylene.

Still other objectives and the utility of the present invention will become apparent as references are made with respect to the following descriptions and the claims thereto.

#### **DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS**

The catalyst of superior catalytic activity and hydrogen sensitivity, capable of producing polymers having high bulk density as provided in the present invention, is produced by a simple yet efficient manufacturing process, which comprises (i) preparing a magnesium solution by contact-reacting a magnesium halide compound, with an alcohol, (ii) reacting the same with an ester compound containing at least one hydroxy group and a silicon compound containing an alkoxy group, and (iii) producing a solid titanium catalyst by adding a titanium compound and a silicon compound.

Types of magnesium halide compounds used in the present invention are as follows: magnesium dihalides such as magnesium chloride, magnesium iodide, magnesium fluoride, and magnesium bromide; alkylmagnesium halides such as methylmagnesium halide, ethylmagnesium halide, propylmagnesium halide, butylmagnesium halide, isobutylmagnesium halide, hexylmagnesium halide, amylmagnesium halide; alkoxymagnesium halides such as methoxymagnesium halide, ethoxymagnesium halide, isopropoxymagnesium halide, butoxymagnesium halide, octoxymagnesium halide; and aryloxymagnesium halides such as

phenoxymagnesium halide and methyl-phenoxymagnesium halide. Of the above magnesium compounds, two or more compounds can be used in a mixture. Further, the above magnesium compounds can be effectively used in the form of a complex compound with other metals.

5 Of the compounds listed above, some can be represented by a simple formula, but the others cannot be so represented depending on the production methods of magnesium compounds. In the latter cases, it can be generally regarded as a mixture of some of the listed compounds. For example, the following compounds can be used in the present invention: such compounds  
10 obtained by reacting magnesium compounds with polysiloxane compounds, silane compounds containing halogen, ester, or alcohol; and such compounds obtained by reacting magnesium metals with alcohol, phenol, or ether in the presence of halosilane, phosphorus pentachloride, or thionyl chloride. However, the preferable magnesium compounds are magnesium halides, especially magnesium chloride or alkylmagnesium chloride, preferably those having an alkyl group of 1 ~ 10 carbons; alkoxymagnesium chlorides, preferably those having 1 ~ 10 carbons;  
15 and aryloxymagnesium chlorides, preferably those having 6 ~ 20 carbons. The magnesium solution used in the present invention is made by dissolving the aforementioned compounds with alcohol as a solvent in the presence or absence of a hydrocarbon solvent.

As to the types of hydrocarbon solvents used in the present invention, they include aliphatic  
20 hydrocarbons such as pentane, hexane, heptane, octane, decane, and kerosene; alicyclic hydrocarbons such as cyclopentane, methylcyclopentane, cyclohexane, and methylcyclohexane; aromatic hydrocarbons such as benzene, toluene, xylene, ethylbenzene, cumene, and cymene; and halogenated hydrocarbons such as dichloropropane, dichloroethylene, trichloroethylene, carbon tetrachloride, and chlorobenzene.

25 When a magnesium compound is converted into a magnesium solution, alcohol is used in the presence or absence of the aforementioned hydrocarbons. The types of alcohol include those containing 1 ~ 20 carbon atoms such as methanol, ethanol, propanol, butanol, pentanol, hexanol, octanol, decanol, dodecanol, octadecyl alcohol, benzyl alcohol, phenylethyl alcohol,  
30 isopropyl benzyl alcohol, and cumyl-alcohol, although alcohols containing 1 ~ 12 carbon atoms are preferable. The average size of a target catalyst and its particle distribution can vary according to the type of alcohol, the total contents, types of magnesium compounds, and the ratio of magnesium to alcohol, etc. Nevertheless, the total amount of alcohol required to obtain the

magnesium solution is at least 0.5 mol per each mole of the magnesium compound, preferably about 1.0 ~ 20 mol, or more preferably about 2.0 ~ 10 mol.

The reaction of a magnesium compound with alcohol for producing magnesium solution is preferably carried out in the presence of hydrocarbon. The reaction temperature, while variable depending on the type and the amount of alcohol, is at least -25°C, preferably -10 ~ 200°C, or more preferably about 0 ~ 150°C. It is preferable to carry out the reaction for about 15 minutes ~ 5 hours, preferably for about 30 minutes ~ 4 hours.

Of the electron donors used in the present invention, the ester compounds containing at least one hydroxy group include unsaturated aliphatic acid esters having at least one hydroxy group such as, 2-hydroxy ethylacrylate, 2-hydroxy ethylmethacrylate, 2-hydroxypropyl acrylate, 2-hydroxypropylmethacrylate, 4-hydroxy butylacrylate, pentaerythritol triacrylate; aliphatic monoesters or polyesters containing at least one hydroxy group such as 2-hydroxy ethyl acetate, methyl 3-hydroxy butylate, ethyl 3-hydroxy butylate, methyl 2-hydroxy isobutylate, ethyl 2-hydroxy isobutylate, methyl 3-hydroxy-2-methyl propionate, 2,2-dimethyl-hydroxy propionate, ethyl-6-hydroxy hexanoate, t-butyl-2-hydroxy isobutylate, diethyl-3-hydroxy glutarate, ethyl lactate, isopropyl lactate, butyl isobutyl lactate, isobutyl lactate, ethyl mandelate, dimethyl ethyl tartrate, ethyl tartrate, dibutyl tartrate, diethyl citrate, triethyl citrate, ethyl-2-hydroxy-caproate, diethyl bis-(hydroxy methyl)malonate; aromatic esters having at least one hydroxy group such as 2-hydroxy ethyl benzoate, 2-hydroxy ethyl salicylate, methyl-4-(hydroxy methyl) benzoate, methyl-4-hydroxy benzoate, ethyl-3-hydroxy benzoate, 4-methyl salicylate, ethyl salicylate, phenyl salicylate, propyl-4-hydroxy benzoate, phenyl-3-hydroxy naphthanoate, monoethylene glycol monobenzoate, diethylene glycol benzoate, triethylene glycol benzoate; alicyclic esters having at least one hydroxy group such as lactone, and others. The amount of the ester compound containing at least one hydroxy group should be 0.001 ~ 5 mol per mole of magnesium, or preferably 0.01 ~ 2 mol per mole of magnesium.

For the silicon compound containing an alkoxy group, the other electron donor in the present invention, a compound having a general formula of  $R^1_nSi(OR^2)_{4-n}$  (here,  $R^1$  and  $R^2$  represents a hydrocarbon having 1 ~ 12 carbons, and n for an integer of 0 ~ 3) is preferable. More specifically, it includes dimethyldimethoxy silane, dimethyldiethoxy silane, diphenyldimethoxy silane, methylphenyldimethoxy silane, diphenyldiethoxy silane,

ethyltrimethoxy silane, vinyltrimethoxy silane, methyltrimethoxy silane, phenyltrimethoxy silane, methyltriethoxy silane, ethyltriethoxy silane, vinyltriethoxy silane, butyltriethoxy silane, phenyltriethoxy silane, ethyltriisopropoxy silane, vinyltributoxy silane, ethyl silicate, butyl silicate, methyltriaryloxy silane, etc. The amount of such compound should be 0.05 ~ 3 mol per mole of magnesium, or more preferably 0.1 ~ 2 mol per mole of magnesium.

As for the temperature for the contact-reaction of a magnesium solution, an ester compound containing at least one hydroxy group, and an alkoxy silicon compound, the temperature of 0 ~ 100°C is appropriate, or more preferably 10 ~ 70°C.

In the process, the catalyst particles are recrystallized by reacting the magnesium compound solution with a mixture of a liquid titanium compound of a general formula of  $Ti(OR)_aX_{4-a}$  (R-stands for an alkyl group with 1 ~ 10 carbons; X for a halogen atom; and "a" for a natural number of 0 to 4) and a silicon compound of a general formula of  $R_nSiCl_{4-n}$  (here R stands for hydrogen; or an alkyl, alkoxy, haloalkyl, or aryl group having 1 to 10 carbons; or a halosilyl or halosilyl alkyl group having 1 to 8 carbons;  $n = 0-3$ ). The types of titanium compounds which satisfy the general formula of  $Ti(OR)_aX_{4-a}$  include titanium tetrahalide such as  $TiCl_4$ ,  $TiBr_4$ , and  $TiI_4$ ; alkoxy titanium trihalide such as  $Ti(OCH_3)Cl_3$ ,  $Ti(OC_2H_5)Cl_3$ ,  $Ti(OC_2H_5)Br_3$ , and  $Ti(O(i-C_4H_9)Br_3$ ; alkoxy titanium dihalide compounds such as  $Ti(OCH_3)_2Cl_2$ ,  $Ti(OC_2H_5)_2Cl_2$ ,  $Ti(O(i-C_4H_9)_2Cl_2$ , and  $Ti(OC_2H_5)_2Br_2$ ; and tetra-alkoxy titaniums such as  $Ti(OCH_3)_4$ ,  $Ti(OC_2H_5)_4$ , and  $Ti(OC_4H_9)_4$ . A mixture of the above titanium compounds can also be used in the present invention. However, the preferable titanium compounds are those containing halogen, or more preferably titanium tetrachloride.

The types of silicon compounds satisfying the above general formula of  $R_nSiCl_{4-n}$  include silicon tetrachloride; trichlorosilanes such as trichlorosilane, methyltrichlorosilane, ethyltrichlorosilane, phenyltrichlorosilane; dichlorosilanes such as dimethyldichlorosilane, diethyldichlorosilane, di-phenyldichlorosilane, and methylphenyldichlorosilane; monochlorosilanes such as trimethylchlorosilane; and a mixture of these silicon compounds can also be used in the present invention, or more preferably silicon tetrachloride can be used.

The amount of the mixture of a titanium compound and a silicon compound used during the re-crystallization of the magnesium compound solution is appropriately 0.1 ~ 200 mol per

mole of the magnesium halide compound, preferably 0.1 ~ 100 mol, or more preferably 0.2 ~ 80 mol. The molar ratio of a titanium compound to a silicon compound in the mixture is appropriately 0.05 ~ 0.95, or more preferably 0.1 ~ 0.8. When the magnesium compound solution is reacted with the mixture of a titanium compound and a silicon compound, the shape and the size of the resultant re-crystallized solid constituents vary a great deal according to the reaction conditions. In order to obtain the target size of the catalyst and the size and distribution of the polymers, as intended by the present invention, it is advantageous to maintain the above mixture amounts for said titanium and silicon compounds, as well as their mix ratios. If it is outside of the above range, it will be difficult to obtain the results as intended. The reaction of the magnesium compound with the mixture of a titanium compound and a silicon compound should be carried out preferably at a sufficiently low temperature to result in formation of solid constituents. More preferably, the reaction should be carried out by contact-reaction at -70 ~ 70°C, or most preferably at -50 ~ 50°C. After the contact-reaction the reacting temperature is slowly raised for sufficient reaction for the duration of 0.5 ~ 5 hours at 50 ~ 150°C.

The particles of the solid catalysts obtained during the above process can be further reacted with titanium compounds. These titanium compounds are titanium halides, and alkoxy titanium halide with an alkoxy functional group of 1 ~ 20 carbons. At times, a mixture of these compounds can also be used. Of these compounds, however, titanium halide and an alkoxy titanium halide compound having an alkoxy functional group of 1~8 carbons can be appropriately used, or more preferably titanium tetrahalide can be used.

Further, the solid complex titanium catalysts produced during the process of the present invention can be utilized during homo-polymerization or co-polymerization of ethylene. In particular, the catalyst is used in homo-polymerization of ethylene, and also in co-polymerization of ethylene and  $\alpha$ -olefin such as propylene, 1-butene, 1-pentene, 1-methyl-1-pentene, or 1-hexene having three or more carbons.

The polymerization reaction in the presence of the catalyst of the present invention is carried out by means of using (i) a solid complex titanium catalyst of the present invention, comprising magnesium, titanium, halogen, and electron donors, and (ii) a cocatalyst comprising, compounds of organic metals of Groups II and III of the Periodic Table.

The solid complex titanium catalyst constituents of the present invention can be used in pre-polymerization of ethylene or  $\alpha$ -olefin prior to the use in the aforementioned polymerization reaction. The pre-polymerization can be carried out in the presence of a hydrocarbon solvent such as hexane, at a sufficiently low temperature, with ethylene or  $\alpha$ -olefin under pressure, in the presence of the above catalyst constituents and such an organic aluminum compound as triethylaluminum. Pre-polymerization, by maintaining the shape of the catalyst by surrounding the catalyst particles with polymers, is helpful in producing food-quality post-polymerization shape of the polymers. The weight ratio of the polymers to the catalysts after pre-polymerization is ordinarily 0.1 : 1 to 20 : 1.

The organometallic compound in the present invention can be represented by a general formula of  $MR_n$ , wherein, M stands for a metal constituent of Group II or IIIA in the Periodic Table, such as magnesium, calcium, zinc, boron, aluminum, and gallium, R for an alkyl group with 1 ~ 20 carbons, such as a methyl, ethyl, butyl, hexyl, octyl, or decyl group, and n for the atomic value of the metal constituent. As for more preferable organometallic compounds, trialkyl aluminum having an alkyl group of 1 ~ 6 carbons, such as triethylaluminum and triisobutylaluminum, or the mixture thereof can be utilized. On occasions, an organic aluminum compound having one or more halogen or hydride groups, such as ethylaluminum dichloride, diethylaluminum chloride, ethyl-aluminum sesqui-chloride, or diisobutylaluminum hydride can also be used.

As for the polymerization reaction, it is possible to carry out either gas phase or bulk polymerization in the absence of an organic solvent, or liquid slurry polymerization in the presence of an organic solvent. These polymerization methods, however, are carried out in the absence of oxygen, water, or other compounds that may act as catalytic poison.

The concentration of the solid complex titanium compound (i) with respect to the polymerization system, in the case of a liquid phase slurry polymerization, is approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the solvent, or more preferably approximately 0.001 ~ 0.5 mmol. As for the solvent, the following compounds or the mixtures thereof can be used: alkanes or cycloalkanes such as pentane, hexane, heptane, n-octane, isooctane, cyclohexane, or methylcyclohexane; alkylaromatic such as toluene, xylene,

ethylbenzene, isopropylbenzene, ethyltoluene, n-propylbenzene, or diethylbenzene; and halogenated aromatics such as chlorobenzene, chloronaphthalene, or ortho-dichlorobenzene.

In the case of gas phase polymerization, the amount of the solid complex titanium catalyst (i) should be approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the polymerization reactant, preferably approximately 0.001 ~ 1.0 mmol, or more preferably approximately 0.01 ~ 0.5 mmol.

The preferable concentration of the organometallic compound (ii) is about 1 - 2,000 mol, as calculated by the aluminum atoms, per mole of the titanium atoms in the catalyst (i), or more preferably about 5 ~ 500 mol.

To secure a high reaction rate of polymerization, the polymerization herein is carried out at a sufficiently high temperature, regardless of the polymerization manufacturing process. Generally, the temperature of approximately 20 ~ 200°C is appropriate, or more preferably approximately 20 ~ 95°C. The appropriate pressure of monomers at the time of polymerization is the atmospheric to 100 atm, or more preferably 2 ~ 50 atm.

In the present invention, in order to evaluate the hydrogen reactivity of the catalyst, the changes in the molecular weight according to the amount of hydrogen at the time of polymerization are shown as a melt index (ASTM D 1238), the index generally known in the art. The value of the melt index generally becomes greater as the molecular weight decreases.

The products obtained by the method of polymerization of the present invention are solid ethylene homogeneous polymers or the copolymers of ethylene and  $\alpha$ -olefin, which have excellent bulk density and fluidity. Since the polymer yields are sufficiently high, there is no need for the removal of the catalyst residues.

The present invention is further described by means of the examples and comparative examples as below but should not be confined or limited to these examples.

#### Example 1

### Production of catalyst

A solid complex titanium catalyst was produced by means of the following three steps:

5 (i) Step: Production of magnesium solution

10 Into a 1.0L reactor equipped with a mechanical stirrer, replaced with nitrogen atmosphere, 9.5 g of  $MgCl_2$  and 400 ml of decane were placed therein. After they were stirred at 300 rpm, 60 ml of 2-ethyl hexanol was added thereto. The temperature was raised to 120 °C, and then the reaction was allowed to continue for three hours. The homogenous solution, which was obtained after the reaction, was cooled to room temperature (25°C).

15 (ii) Step : Contact-reaction of a magnesium solution, an ester containing a hydroxy group and an alkoxy boron compound

To the magnesium solution, cooled to room temperature as above, 1.2 ml of 2-hydroxyethyl methacrylate and 10 ml (45 mmol) of silicon tetraethoxide were added, and then the reaction was allowed to continue for an hour.

20 (iii) Step : Treatment of a mixture of a titanium compound and a silicon compound

25 After cooling the above solution to room temperature (25°C), a solution mixture of 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride was dripped into the above solution for one hour. After the completion of the dripping process, the temperature of the reactor was raised to 90°C while stirring, after which was maintained at that temperature for one hour. After stopping the stirring, the supernatant of the solution was removed, and to the remaining solid layer was added 300 ml of decane and 100 ml of titanium tetrachloride in sequence. There, the temperature was raised to 100°C and maintained thereat for two hours. After the reaction, the reactor was cooled to room temperature and the washing of the resulting solid product with 400ml of hexane was repeated until the removal of free unreacted titanium chloride. The titanium content of the solid catalyst so produced was 3.6%.

## Polymerization

5 A 2-L high-pressure reactor was dried in an oven and assembled while still hot. In order  
to make the inside of the reactor nitrogen atmosphere, nitrogen and vacuum were  
alternatively manipulated three times in the reactor. To the reactor was added 1,000 ml of n-  
hexane, after which 2 mmols of triethylaluminum and a solid catalyst by 0.03 mmol in terms  
of the titanium atoms were added thereto. Then, 2000 ml of hydrogen was added. The  
temperature was raised to 80°C while stirring at 700 rpm. The pressure of ethylene was  
10 adjusted to 80 psi, and the polymerization was allowed to continue for an hour. After the  
polymerization, the temperature of the reactor was lowered to room temperature, and a large  
amount of ethanol was added to stop the polymerization. The polymer thus produced was  
collected by separation and was dried in an oven at 50°C for at least six hours, whereby  
polyethylene was obtained in the form of white powder.

The polymerization activity (kg of polyethylene divided by mmol of Ti) was calculated as  
the weight (kg) ratio of the polymer as produced per the amount of the catalysts so used  
(mmol of Ti). The results of the polymerization are shown in Table 1, together with the bulk  
density (g/ ml) of the polymers and the melt index (g/10 minutes).

### Example 2

25 The catalyst was prepared the same as in Example 1, except that in Step (ii) of Example 1,  
the temperature of the magnesium solution was adjusted to room temperature (25°C). The  
titanium content of the catalyst thus produced was 3.2 %. The polymerization was carried out as  
in Example 1, and the results thereof are shown in Table 1.

### Example 3

30 The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2,  
2.4 ml of 2-hydroxyethyl methacrylate and 10.0 ml of silicon tetraethoxide were used. The

titanium content of the catalyst thus produced was 2.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 4

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 3.6 ml of 2-hydroxyethyl methacrylate and 10.0 ml of silicon tetraethoxide were used. The titanium content of the catalyst thus produced was 2.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 5

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 1.2 ml of 2-hydroxyethyl methacrylate and 5.0 ml of silicon tetraethoxide were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 6

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 1.2 ml of 2-hydroxyethyl methacrylate and 15.0 ml of silicon tetraethoxide were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.1 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 7

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride were dripped in the period of 30 minutes for production of the catalyst. The titanium content of the catalyst thus produced was 3.8 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 8

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride were dripped in the period of 2 hours for production of the catalyst. The titanium content of the catalyst thus produced was 3.6 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 9

The polymerization was carried out using the catalyst produced in Example 1 and 1500 ml of hydrogen, and the results thereof are shown in Table 1.

Example 10

The polymerization was carried out using the catalyst produced in Example 1 and 1000 ml of hydrogen, and the results thereof are shown in Table 1.

Example 11

The catalyst was prepared the same as in Example 2, except that in Step (i) of Example 2, 400 ml of decane was used in the production of the magnesium solution. The titanium content of the catalyst thus produced was 3.6 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 12

The catalyst was prepared the same as in Example 11, except that in Step (iii) of Example 11, 40 ml of titanium tetrachloride and 20 ml of silicon tetrachloride were used. The titanium content of the catalyst thus produced was 3.8 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

### Example 13

The catalyst was prepared the same as in Example 12, except that in Step (iii) of Example 12, 20 ml of titanium tetrachloride and 40 ml of silicon tetrachloride were used. The titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

### Example 14

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 40 ml of titanium tetrachloride and 20 ml of silicon tetrachloride were used. The titanium content of the catalyst thus produced was 3.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

### Example 15

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 20 ml of titanium tetrachloride and 40 ml of silicon tetrachloride were used. The titanium content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

### Comparative Example 1

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 10.0 ml of silicon tetraethoxide was added and 2-hydroxyethyl methacrylate was not used. The titanium content of the catalyst thus produced was 3.8 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

### Comparative Example 2

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 1.2 ml of 2-hydroxyethyl methacrylate was added and silicon tetraethoxide was not used. The

titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Comparative Example 3

5

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, neither 2-hydroxyethyl methacrylate nor silicon tetraethoxide was used. The titanium content of the catalyst thus produced was 4.3 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

10

#### Comparative Example 4

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 60 ml of titanium tetrachloride was used. The titanium content of the catalyst thus produced was 4.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

15

#### Comparative Example 5

The polymerization was carried out using the catalyst produced in Comparative Example 4 and 1500 ml of hydrogen. The results thereof are shown in Table 1.

20

#### Comparative Example 6

The polymerization was carried out using the catalyst produced in Comparative Example 4 and 1000 ml of hydrogen. The results thereof are shown in Table 1.

25

#### Comparative Example 7

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, neither 2-hydroxyethyl methacrylate nor silicon tetraethoxide was used, and in Step (iii) 60 ml of titanium tetrachloride was used. The titanium content of the catalyst thus produced was 4.1 %.

30

The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Table 1

Results of Polymerization

| Example | Amount of Hydrogen (ml) | Activity (kg PE/mmol Ti) | Bulk Density (g/ml) | Melting Index (g/10min) |
|---------|-------------------------|--------------------------|---------------------|-------------------------|
| 1       | 2.000                   | 2.3                      | 0.36                | 38.9                    |
| 2       | 2.000                   | 2.1                      | 0.35                | 35.2                    |
| 3       | 2.000                   | 2.5                      | 0.34                | 38.4                    |
| 4       | 2.000                   | 2.3                      | 0.33                | 39.2                    |
| 5       | 2.000                   | 2.6                      | 0.34                | 33.1                    |
| 6       | 2.000                   | 2.0                      | 0.36                | 32.4                    |
| 7       | 2.000                   | 2.7                      | 0.32                | 38.1                    |
| 8       | 2.000                   | 2.1                      | 0.35                | 34.8                    |
| 9       | 1.500                   | 2.8                      | 0.34                | 19.8                    |
| 10      | 1.000                   | 3.9                      | 0.32                | 3.8                     |
| 11      | 2.000                   | 2.2                      | 0.34                | 36.4                    |
| 12      | 2.000                   | 2.4                      | 0.35                | 31.7                    |
| 13      | 2.000                   | 2.0                      | 0.33                | 34.8                    |
| 14      | 2.000                   | 2.6                      | 0.36                | 38.9                    |
| 15      | 2.000                   | 2.4                      | 0.35                | 36.8                    |
| CE1     | 2.000                   | 1.4                      | 0.35                | 12.4                    |
| CE2     | 2.000                   | 1.6                      | 0.32                | 22.6                    |
| CE3     | 2.000                   | 1.2                      | 0.28                | 8.2                     |
| CE4     | 2.000                   | 2.2                      | 0.32                | 18.1                    |
| CE5     | 1.500                   | 2.9                      | 0.32                | 7.8                     |
| CE6     | 1.000                   | 3.6                      | 0.31                | 2.7                     |
| CE7     | 2.000                   | 1.1                      | 0.22                | 7.8                     |

\* CE : Comparative Examples

As shown above, the production process of the catalyst of the present invention for homo-polymerization and co-polymerization of ethylene is simple with excellent catalytic activity.

Further, with the catalyst particles being controlled, high bulk density of the polymer can be provided, and the hydrogen sensitivity is greatly improved..

## ABSTRACT

The present invention relates to a catalyst for homo-polymerization or co-polymerization of ethylene, or more particularly to a solid complex titanium catalyst for homo-polymerization or co-polymerization of ethylene. The catalyst may be produced by preparing a magnesium solution by contact-reacting a magnesium halide compound with alcohol. Reacting the solution with an ester compound and a silicon compound. Then reacting the solution with a mixture of a titanium compound and a silicon compound.

A CATALYST FOR ETHYLENE HOMO AND CO-POLYMERIZATIONBACKGROUND OF THE INVENTIONTechnical Field 1. FIELD OF THE INVENTION

5 The present invention relates to a catalyst for homo-polymerization or co-polymerization of ethylene, or more particularly to a high-activity titanium solid complex catalyst supported in a carrier containing magnesium, ~~said the~~ catalyst showing high catalytic activity, high bulk density, and high hydrogen sensitivity.

Background of the Invention 2. DESCRIPTION OF THE RELATED ART

10 Catalysts containing magnesium for polymerization or co-polymerization of ethylene are known to have very high catalytic activities and to accord good bulk density, which are in turn suitable for liquid phase or gas phase polymerization. By liquid phase polymerization of ethylene, it denotes the polymerization process performed in such medium of bulk ethylene, isopentane, or hexane, and as for the important characteristics in consideration of the applicability of the catalyst used in this process, they are as follows: high activity, bulk density, the amount of molecules of low molecular weight dissolved in a medium, etc. Furthermore, in  
20 most of these manufacturing processes, hydrogen is used to control the molecular weight. The changes in the molecular weight (hereinafter hydrogen sensitivity) according to the amount of hydrogen is another characteristic of a catalyst, which is different per catalyst. The catalyst with high hydrogen sensitivity can control the molecular weight by using less amount of hydrogen at the time of the application of the process. As such, it provides more leeway with respect to the  
25 operation of the process.

30 Many of the titanium-based catalysts containing magnesium for olefin polymerization, and the manufacturing methods thereof have been reported. Especially, many processes making use of magnesium solutions to obtain olefin polymerization catalysts of good bulk density have been known. There is a means of obtaining a magnesium solution by reacting magnesium compounds with such electron donors as alcohol, amine, cyclic ether, or organic carboxylic acid in the presence of a hydrocarbon solvent. As for the cases of use of alcohol, they are disclosed

in US Patent Nos. 4,330,649, and 5,106,807. Further, the methods for production of catalysts containing magnesium by reacting a liquid magnesium solution with a halogenated compound halide compound such as titanium tetrachloride are well known. Such catalysts provide good bulk density, but there is much yet to be improved with respect to their catalytic activities and hydrogen sensitivity. In US Patent Nos. 4,477,639 and 4,518,706, a cyclic ether, tetrahydrofuran was used as a solvent of the magnesium compound.

US Patent Nos. 4,847,227, 4,816,433, 4,829,037, 4,970,186, and 5,130,284 claimed the methods of producing olefin polymerization catalysts of good bulk density, with superior polymerization activity due to the reaction of a titanium chloride compound with an electron donor compound such as magnesium alkoxide, dialkyl phthalate, and phthaloyl chloride.

US Patent No. 5,459,116 reports the method of producing supported titanium solid catalysts by means of contact-reacting a titanium compound and a magnesium solution containing an ester having at least one hydroxy group as an electron donor. By using this method, it is possible to obtain a catalyst of superior polymerization activity and bulk density. However, there remain things to be improved with respect to hydrogen sensitivity.

US Patent No. 5,869,418 shows the method of increasing hydrogen sensitivity by using a dialkoxyphenylalkane in the propylene polymerization as an external electron donor, and the advantages of such method. However, the above effects were obtained by using the external electron donor in addition to the solid catalyst, and also it is limited to polymerization and copolymerization of propylene.

#### ~~Summary of the Invention~~ SUMMARY OF THE INVENTION

As shown above, there is a need for the development of a new catalyst for homopolymerization or co-polymerization of ethylene for producing polymers with the following conditions: simple manufacturing process, high polymerization activity, high bulk density for polymers by means of controlling the catalyst particles, and high hydrogen sensitivity. In the present invention, therefore, it is intended to provide a method for producing, from low-cost compounds via a simple process, a catalyst having an excellent catalytic activity, and superior

hydrogen sensitivity, capable of producing polymers of good bulk density. Further, the specific production process of catalysts and the steps thereof as disclosed in the present invention have never been reported in the prior art.

Consequently, the objective of the present invention is to provide a new catalyst solid component for homo-polymerization or co-polymerization of ethylene, said catalyst having superior catalytic activity and hydrogen sensitivity, capable of producing polymers of high bulk density. More specifically, the objective of the present invention lies in providing a catalyst solid component for homo-polymerization or co-polymerization of ethylene, having a superior hydrogen sensitivity, wherein the form of the catalyst particles are controlled therein.

Another objective of the present invention is to provide a simple process for producing a catalyst for homo-polymerization or co-polymerization of ethylene.

Still other objectives and the utility of the present invention will become apparent as references are made with respect to the following descriptions and the claims thereto.

~~Detailed Description of the Preferred Embodiments~~DETAILED DESCRIPTION OF THE  
PREFERRED EMBODIMENTS

The catalyst of superior catalytic activity and hydrogen sensitivity, capable of producing polymers having high bulk density as provided in the present invention, is produced by a simple yet efficient manufacturing process, which comprises (i) preparing a magnesium solution by contact-reacting a ~~halogenated-magnesium~~magnesium halide compound, with an alcohol, (ii) reacting the same with an ester compound containing at least one hydroxy group and a silicon compound containing an alkoxy group, and (iii) producing a solid titanium catalyst by adding a titanium compound and a silicon compound.

Types of ~~halogenated-magnesium~~magnesium halide compounds used in the present invention are as follows: ~~di-halogenated-magnesium~~magnesium dihalides such as magnesium chloride, magnesium iodide, magnesium fluoride, and magnesium bromide; ~~alkylmagnesium~~alkylmagnesium halides such as methylmagnesium halide, ethylmagnesium halide, propylmagnesium halide, butylmagnesium halide, isobutylmagnesium halide, hexylmagnesium

halide, alkylmagnesium halide; alkoxymagnesium halides such as methoxymagnesium halide, ethoxymagnesium halide, isopropoxymagnesium halide, butoxymagnesium halide, octoxymagnesium halide; and aryloxymagnesium halides such as phenoxymagnesium halide and methyl-phenoxymagnesium halide. Of the above magnesium compounds, two or more compounds can be used in a mixture. Further, the above magnesium compounds can be effectively used in the form of a complex compound with other metals.

Of the compounds listed above, some can be represented by a simple formula, but the others cannot be so represented depending on the production methods of magnesium compounds.

In the latter cases, it can be generally regarded as a mixture of some of the listed compounds. For example, the following compounds can be used in the present invention: such compounds obtained by reacting magnesium compounds with polysiloxane compounds, silane compounds containing halogen, ester, or alcohol; and such compounds obtained by reacting magnesium metals with alcohol, phenol, or ether in the presence of halosilane, phosphorus pentachloride, or thionyl chloride. However, the preferable magnesium compounds are magnesium halides, especially magnesium chloride or alkylmagnesium chloride, preferably those having an alkyl group of 1 ~ 10 carbons; alkoxymagnesium chlorides, preferably those having 1 ~ 10 carbons; and aryloxymagnesium chlorides, preferably those having 6 ~ 20 carbons. The magnesium solution used in the present invention is made by dissolving the aforementioned compounds with alcohol as a solvent in the presence or absence of a hydrocarbon solvent.

As to the types of hydrocarbon solvents used in the present invention, they include aliphatic hydrocarbons such as pentane, hexane, heptane, octane, decane, and kerosene; alicyclic hydrocarbons such as cyclobenzene, ~~methylecyclobenzene~~ cyclopentane, methylcyclopentane, cyclohexane, and methylcyclohexane; aromatic hydrocarbons such as benzene, toluene, xylene, ethylbenzene, cumene, and cymene; and halogenated hydrocarbons such as dichloropropane, dichloroethylene, trichloroethylene, carbon tetrachloride, and chlorobenzene.

When a magnesium compound is converted into a magnesium solution, alcohol is used in the presence or absence of the aforementioned hydrocarbons. The types of alcohol include those containing 1 ~ 20 carbon atoms such as methanol, ethanol, propanol, butanol, pentanol,

hexanol, octanol, decanol, dodecanol, octadecyl alcohol, benzyl alcohol, phenylethyl alcohol, isopropyl benzyl alcohol, and cumyl-alcohol, although alcohols containing 1 ~ 12 carbon atoms are preferable. The average size of a target catalyst and its particle distribution can vary according to the type of alcohol, the total contents, types of magnesium compounds, and the ratio of magnesium to alcohol, etc. Nevertheless, the total amount of alcohol required to obtain the magnesium solution is at least 0.5 mol per each mole of the magnesium compound, preferably about 1.0 ~ 20 mol, or more preferably about 2.0 ~ 10 mol.

The reaction of a magnesium compound with alcohol for producing magnesium solution is preferably carried out in the presence of hydrocarbon. The reaction temperature, while variable depending on the type and the amount of alcohol, is at least -25°C, preferably -10 ~ 200°C, or more preferably about 0 ~ 150°C. It is preferable to carry out the reaction for about 15 minutes ~ 5 hours, preferably for about 30 minutes ~ 4 hours.

Of the electron donors used in the present invention, the ester compounds containing at least one hydroxy group include unsaturated aliphatic acid esters having at least one hydroxy group such as, 2-hydroxy ethylacrylate, 2-hydroxy ethylmethacrylate, 2-hydroxypropyl acrylate, 2-hydroxypropylmethacrylate, 4-hydroxy butylacrylate, pentaerithritol triacrylate; aliphatic monoesters or polyesters containing at least one hydroxy group such as 2-hydroxy ethyl acetate, methyl 3-hydroxy butylate, ethyl 3-hydroxy butylate, methyl 2-hydroxy isobutylate, ethyl 2-hydroxy isobutylate, methyl 3-hydroxy-2-methyl propionate, 2,2-dimethyl-hydroxy propionate, ethyl-6-hydroxy hexanoate, t-butyl-2-hydroxy isobutylate, diethyl-3-hydroxy glutarate, ethyl lactate, isopropyl lactate, butyl isobutyl lactate, isobutyl lactate, ethyl mandelate, dimethyl ethyl tartrate, ethyl tartrate, dibutyl tartrate, diethyl citrate, triethyl citrate, ethyl-2-hydroxy-caproate, diethyl bis-(hydroxy methyl)malonate; aromatic esters having at least one hydroxy group such as 2-hydroxy ethyl benzoate, 2-hydroxy ethyl salicylate, methyl-4-(hydroxy methyl) benzoate, methyl-4-hydroxy benzoate, ethyl-3-hydroxy benzoate, 4-methyl salicylate, ethyl salicylate, phenyl salicylate, propyl-4-hydroxy benzoate, phenyl-3-hydroxy naphthanoate, monoethylene glycol monobenzoate, diethylene glycol benzoate, triethylene glycol benzoate; alicyclic esters having at least one hydroxy group such as lactone, and others. The amount of the ester compound containing at least one hydroxy group should be 0.001 ~ 5 mol per mole of magnesium, or preferably 0.01 ~ 2 mol per mole of magnesium.

For the silicon compound containing an alkoxy group, the other electron donor in the present invention, a compound having a general formula of  $R^1_nSi(OR^2)_{4-n}$  (here,  $R^1$  and  $R^2$  represents a hydrocarbon having 1 ~ 12 carbons, and n for an integer of 0 ~ 3) is preferable.

5 More specifically, it includes dimethyldimethoxy silane, dimethyldiethoxy silane, diphenyldimethoxy silane, methylphenyldimethoxy silane, diphenyldiethoxy silane, ethyltrimethoxy silane, vinyltrimethoxy silane, methyltrimethoxy silane, phenyltrimethoxy silane, methyltriethoxy silane, ethyltriethoxy silane, vinyltriethoxy silane, butyltriethoxy silane, phenyltriethoxy silane, ethyltriisopropoxy silane, vinyltributoxy silane, ethyl silicate, butyl  
10 silicate, methyltriaryloxy silane, etc. The amount of such compound should be 0.05 ~ 3 mol per mole of magnesium, or more preferably 0.1 ~ 2 mol per mole of magnesium.

As for the temperature for the contact-reaction of a magnesium solution, an ester compound containing at least one hydroxy group, and an alkoxy silicon compound, the temperature of 0 ~  
15 100°C is appropriate, or more preferably 10 ~ 70°C.

In the process, the catalyst particles are recrystallized by reacting the magnesium compound solution with a mixture of a liquid titanium compound of a general formula of  $Ti(OR)_aX_{4-a}$  (R-stands for an alkyl group with 1 ~ 10 carbons; X for a halogen atom; and "a" for a  
20 natural number of 0 to 4) and a silicon compound of a general formula of  $R_nSiCl_{4-n}$  (here R stands for hydrogen; or an alkyl, alkoxy, haloalkyl, or aryl group having 1 to 10 carbons; or a halosilyl or halosilyl alkyl group having 1 to 8 carbons; n = 0-3). The types of titanium compounds which satisfy the general formula of  $Ti(OR)_aX_{4-a}$  include 4-halogenated  
~~titanium~~ titanium tetrahalide such as  $TiCl_4$ ,  $TiBr_4$ , and  $TiI_4$ ; ~~3-halogenated alkoxy titanium~~ alkoxy  
25 titanium trihalide such as  $Ti(OCH_3)Cl_3$ ,  $Ti(OC_2H_5)Cl_3$ ,  $Ti(OC_2H_5)Br_3$ , and  $Ti(O(i-C_4H_9))Br_3$ ;  
~~2-halogenated alkoxy titanium~~ alkoxy titanium dihalide compounds such as  $Ti(OCH_3)_2Cl_2$ ,  
 $Ti(OC_2H_5)_2Cl_2$ ,  $Ti(O(i-C_4H_9))_2Cl_2$ , and  $Ti(OC_2H_5)_2Br_2$ ; and tetra-alkoxy titaniums such as  
 $Ti(OCH_3)_4$ ,  $Ti(OC_2H_5)_4$ , and  $Ti(OC_4H_9)_4$ . A mixture of the above titanium compounds can also  
30 be used in the present invention. However, the preferable titanium compounds are those containing halogen, or more preferably titanium tetrachloride.

The types of silicon compounds satisfying the above general formula of  $R_nSiCl_{4-n}$  include silicon tetrachloride; trichlorosilanes such as trichlorosilane, methyltrichlorosilane, ethyltrichlorosilane, phenyltrichlorosilane; dichlorosilanes such as dimethylchlorosilane, dimethyldichlorosilane, diethyldichlorosilane, di-phenyldichlorosilane, and methylphenyldichlorosilane; monochlorosilanes such as trimethylchlorosilane; and a mixture of these silicon compounds can also be used in the present invention, or more preferably silicon tetrachloride can be used.

The amount of the mixture of a titanium compound and a silicon compound used during the re-crystallization of the magnesium compound solution is appropriately 0.1 ~ 200 mol per mole of the ~~halogenated magnesium~~ magnesium halide compound, preferably 0.1 ~ 100 mol, or more preferably 0.2 ~ 80 mol. The molar ratio of a titanium compound to a silicon compound in the mixture is appropriately 0.05 ~ 0.95, or more preferably 0.1 ~ 0.8. When the magnesium compound solution is reacted with the mixture of a titanium compound and a silicon compound, the shape and the size of the resultant re-crystallized solid constituents vary a great deal according to the reaction conditions. In order to obtain the target size of the catalyst and the size and distribution of the polymers, as intended by the present invention, it is advantageous to maintain the above mixture amounts for said titanium and silicon compounds, as well as their mix ratios. If it is outside of the above range, it will be difficult to obtain the results as intended. The reaction of the magnesium compound with the mixture of a titanium compound and a silicon compound should be carried out preferably at a sufficiently low temperature to result in formation of solid constituents. More preferably, the reaction should be carried out by contact-reaction at -70 ~ 70°C, or most preferably at -50 ~ 50°C. After the contact-reaction the reacting temperature is slowly raised for sufficient reaction for the duration of 0.5 ~ 5 hours at 50 ~ 150°C.

The particles of the solid catalysts obtained during the above process can be further reacted with titanium compounds. These titanium compounds are titanium halides, and ~~halogenated alkoxy titanium~~ alkoxy titanium halide with an alkoxy functional group of 1 ~ 20 carbons. At times, a mixture of these compounds can also be used. Of these compounds, however, titanium halide and ~~an halogenated alkoxy titanium~~ alkoxy titanium halide compound having an alkoxy

functional group of 1~8 carbons can be appropriately used, or more preferably titanium tetrahalide can be used.

Further, the solid complex titanium catalysts produced during the process of the present invention can be utilized during homo-polymerization or co-polymerization of ethylene. In particular, the catalyst is used in homo-polymerization of ethylene, and also in co-polymerization of ethylene and  $\alpha$ -olefin such as propylene, 1-butene, 1-pentene, 1-methyl-1-pentene, or 1-hexene having three or more carbons.

The polymerization reaction in the presence of the catalyst of the present invention is carried out by means of using (i) a solid complex titanium catalyst of the present invention, comprising magnesium, titanium, halogen, and electron donors, and (ii) a cocatalyst comprising, compounds of organic metals of Groups II and III of the Periodic Table.

The solid complex titanium catalyst constituents of the present invention can be used in pre-polymerization of ethylene or  $\alpha$ -olefin prior to the use in the aforementioned polymerization reaction. The pre-polymerization can be carried out in the presence of a hydrocarbon solvent such as hexane, at a sufficiently low temperature, with ethylene or  $\alpha$ -olefin under pressure, in the presence of the above catalyst constituents and such an organic aluminum compound as triethylaluminum. Pre-polymerization, by maintaining the shape of the catalyst by surrounding the catalyst particles with polymers, is helpful in producing food-quality post-polymerization shape of the polymers. The weight ratio of the polymers to the catalysts after pre-polymerization is ordinarily 0.1 : 1 to 20 : 1.

The organometallic compound in the present invention can be represented by a general formula of  $MR_n$ , wherein, M stands for a metal constituent of Group II or IIIA in the Periodic Table, such as magnesium, calcium, zinc, boron, aluminum, and gallium, R for an alkyl group with 1 ~ 20 carbons, such as a methyl, ethyl, butyl, hexyl, octyl, or decyl group, and n for the atomic value of the metal constituent. As for more preferable organometallic compounds, trialkyl aluminum having an alkyl group of 1 ~ 6 carbons, such as triethylaluminum and triisobutylaluminum, or the mixture thereof can be utilized. On occasions, an organic aluminum compound having one or more halogen or hydride groups, such as ethylaluminum dichloride,

diethylaluminum chloride, ethyl-aluminum sesqui-chloride, or diisobutylaluminum hydride can also be used.

As for the polymerization reaction, it is possible to carry out either gas phase or bulk polymerization in the absence of an organic solvent, or liquid slurry polymerization in the presence of an organic solvent. These polymerization methods, however, are carried out in the absence of oxygen, water, or other compounds that may act as catalytic poison.

The concentration of the solid complex titanium compound (i) with respect to the polymerization system, in the case of a liquid phase slurry polymerization, is approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the solvent, or more preferably approximately 0.001 ~ 0.5 mmol. As for the solvent, the following compounds or the mixtures thereof can be used: alkanes or cycloalkanes such as pentane, hexane, heptane, n-octane, isooctane, cyclohexane, or methylcyclohexane; alkylaromatic such as toluene, xylene, ethylbenzene, isopropylbenzene, ethyltoluene, n-propylbenzene, or diethylbenzene; and halogenated aromatics such as chlorobenzene, chloronaphthalene, or ortho-dichlorobenzene.

In the case of gas phase polymerization, the amount of the solid complex titanium catalyst (i) should be approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the polymerization reactant, preferably approximately 0.001 ~ 1.0 mmol, or more preferably approximately 0.01 ~ 0.5 mmol.

The preferable concentration of the organometallic compound (ii) is about 1 - 2,000 mol, as calculated by the aluminum atoms, per mole of the titanium atoms in the catalyst (i), or more preferably about 5 ~ 500 mol.

To secure a high reaction rate of polymerization, the polymerization herein is carried out at a sufficiently high temperature, regardless of the polymerization manufacturing process. Generally, the temperature of approximately 20 ~ 200°C is appropriate, or more preferably approximately 20 ~ 95°C. The appropriate pressure of monomers at the time of polymerization is the atmospheric to 100 atm, or more preferably 2 ~ 50 atm.

In the present invention, in order to evaluate the hydrogen reactivity of the catalyst, the changes in the molecular weight according to the amount of hydrogen at the time of polymerization are shown as a melt index (ASTM D 1238), the index generally known in the art. The value of the melt index generally becomes greater as the molecular weight decreases.

5

The products obtained by the method of polymerization of the present invention are solid ethylene homogeneous polymers or the copolymers of ethylene and  $\alpha$ -olefin, which have excellent bulk density and fluidity. Since the polymer yields are sufficiently high, there is no need for the removal of the catalyst residues.

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The present invention is further described by means of the examples and comparative examples as below but should not be confined or limited to these examples.

#### Example 1

##### Production of catalyst

A solid complex titanium catalyst was produced by means of the following three steps:

##### (i) Step: Production of magnesium solution

Into a 1.0L reactor equipped with a mechanical stirrer, replaced with nitrogen atmosphere, 9.5 g of  $MgCl_2$  and 400 ml of decane were placed therein. After they were stirred at 300 rpm, 60 ml of 2-ethyl hexanol was added thereto. The temperature was raised to 120 °C, and then the reaction was allowed to continue for three hours. The homogenous solution, which was obtained after the reaction, was cooled to room temperature (25°C).

(ii) Step : Contact-reaction of a magnesium solution, an ester containing a hydroxy group and an alkoxy boron compound

To the magnesium solution, cooled to room temperature as above, 1.2 ml of 2-hydroxyethyl methacrylate and 10 ml (45 mmol) of silicon tetraethoxide were added, and then the reaction was allowed to continue for an hour.

5 (iii) Step : Treatment of a mixture of a titanium compound and a silicon compound

10 After cooling the above solution to room temperature (25°C), a solution mixture of 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride was dripped into the above solution for one hour. After the completion of the dripping process, the temperature of the reactor was raised to 90°C while stirring, after which was maintained at that temperature for one hour. After stopping the stirring, the supernatant of the solution was removed, and to the remaining solid layer was added 300 ml of decane and 100 ml of titanium tetrachloride in sequence. There, the temperature was raised to 100°C and maintained thereat for two hours. After the reaction, the reactor was cooled to room temperature and the washing of the resulting solid product with 400ml of hexane was repeated until the removal of free unreacted titanium chloride. The titanium content of the solid catalyst so produced was 3.6%.

15 Polymerization

20 A 2-L high-pressure reactor was dried in an oven and assembled while still hot. In order to make the inside of the reactor nitrogen atmosphere, nitrogen and vacuum were alternatively manipulated three times in the reactor. To the reactor was added 1,000 ml of n-hexane, after which 2 mmols of triethylaluminum and a solid catalyst by 0.03 mmol in terms of the titanium atoms were added thereto. Then, 2000 ml of hydrogen was added. The temperature was raised to 80°C while stirring at 700 rpm. The pressure of ethylene was adjusted to 80 psi, and the polymerization was allowed to continue for an hour. After the polymerization, the temperature of the reactor was lowered to room temperature, and a large amount of ethanol was added to stop the polymerization. The polymer thus produced was collected by separation and was dried in an oven at 50°C for at least six hours, whereby polyethylene was obtained in the form of white powder.

The polymerization activity (kg of polyethylene divided by mmol of Ti) was calculated as the weight (kg) ratio of the polymer as produced per the amount of the catalysts so used (mmol of Ti). The results of the polymerization are shown in Table 1, together with the bulk density (g/ ml) of the polymers and the melt index (g/10 minutes).

5

#### Example 2

The catalyst was prepared the same as in Example 1, except that in Step (ii) of Example 1, the temperature of the magnesium solution was adjusted to room temperature (25°C). The titanium content of the catalyst thus produced was 3.2 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

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#### Example 3

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 2.4 ml of 2-hydroxyethyl methacrylate and 10.0 ml of silicon tetraethoxide were used. The titanium content of the catalyst thus produced was 2.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

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#### Example 4

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 3.6 ml of 2-hydroxyethyl methacrylate and 10.0 ml of silicon tetraethoxide were used. The titanium content of the catalyst thus produced was 2.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

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#### Example 5

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 1.2 ml of 2-hydroxyethyl methacrylate and 5.0 ml of silicon tetraethoxide were used for the

30

production of the catalyst. The titanium content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 6

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 1.2 ml of 2-hydroxyethyl methacrylate and 15.0 ml of silicon tetraethoxide were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.1 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 7

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride were dripped in the period of 30 minutes for production of the catalyst. The titanium content of the catalyst thus produced was 3.8 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 8

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride were dripped in the period of 2 hours for production of the catalyst. The titanium content of the catalyst thus produced was 3.6 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 9

The polymerization was carried out using the catalyst produced in Example 1 and 1500 ml of hydrogen, and the results thereof are shown in ~~Table 1~~ Table 1.

Example 10

The polymerization was carried out using the catalyst produced in Example 1 and 1000 ml of hydrogen, and the results thereof are shown in Table 1.

Example 11

The catalyst was prepared the same as in Example 2, except that in Step (i) of Example 2, 400 ml of decane was used in the production of ~~magnesium solution~~ of the magnesium solution.

The titanium content of the catalyst thus produced was 3.6 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 12

The catalyst was prepared the same as in Example 11, except that in Step (iii) of Example 11, 40 ml of titanium tetrachloride and 20 ml of silicon tetrachloride were used. The titanium content of the catalyst thus produced was 3.8 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 13

The catalyst was prepared the same as in Example 12, except that in Step (iii) of Example 12, 20 ml of titanium tetrachloride and 40 ml of silicon tetrachloride were used. The titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 14

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 40 ml of titanium tetrachloride and 20 ml of silicon tetrachloride were used. The titanium content of the catalyst thus produced was 3.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 15

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2,  
5 20 ml of titanium tetrachloride and 40 ml of silicon tetrachloride were used. The titanium  
content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in  
Example 1, and the results thereof are shown in Table 1.

Comparative Example 1

10 The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2,  
10.0 ml of silicon tetraethoxide was added and 2-hydroxyethyl methacrylate was not used.  
The titanium content of the catalyst thus produced was 3.8 %. The polymerization was carried  
out as in Example 1, and the results thereof are shown in Table 1.

Comparative Example 2

15 The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2,  
1.2 ml of 2-hydroxyethyl methacrylate was added and silicon tetraethoxide was not used. The  
20 titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as  
in Example 1, and the results thereof are shown in Table 1.

Comparative Example 3

25 The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2,  
neither 2-hydroxyethyl methacrylate nor silicon tetraethoxide was used. The titanium content  
of the catalyst thus produced was 4.3 %. The polymerization was carried out as in Example 1,  
and the results thereof are shown in Table 1.

30 Comparative Example 4

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 60 ml of titanium tetrachloride was used. The titanium content of the catalyst thus produced was 4.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

5

#### Comparative Example 5

The polymerization was carried out using the catalyst produced in Comparative Example 4 and 1500 ml of hydrogen. The results thereof are shown in Table 1.

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#### Comparative Example 6

The polymerization was carried out using the catalyst produced in Comparative Example 4 and 1000 ml of hydrogen. The results thereof are shown in Table 1.

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#### Comparative Example 7

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, neither 2-hydroxyethyl methacrylate nor silicon tetraethoxide was used, and in Step (iii) 60 ml of titanium tetrachloride was used. The titanium content of the catalyst thus produced was 4.1 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

25

Table 1  
Results of Polymerization

| Example | Amount of<br>Hydrogen<br>(ml) | Activity<br>(kg PE/mmol Ti) | Bulk Density<br>(g/ml) | Melting Index<br>(g/10min) |
|---------|-------------------------------|-----------------------------|------------------------|----------------------------|
| 1       | 2.000                         | 2.3                         | 0.36                   | 38.9                       |
| 2       | 2.000                         | 2.1                         | 0.35                   | 35.2                       |
| 3       | 2.000                         | 2.5                         | 0.34                   | 38.4                       |
| 4       | 2.000                         | 2.3                         | 0.33                   | 39.2                       |
| 5       | 2.000                         | 2.6                         | 0.34                   | 33.1                       |

|     |       |     |      |      |
|-----|-------|-----|------|------|
| 6   | 2.000 | 2.0 | 0.36 | 32.4 |
| 7   | 2.000 | 2.7 | 0.32 | 38.1 |
| 8   | 2.000 | 2.1 | 0.35 | 34.8 |
| 9   | 1.500 | 2.8 | 0.34 | 19.8 |
| 10  | 1.000 | 3.9 | 0.32 | 3.8  |
| 11  | 2.000 | 2.2 | 0.34 | 36.4 |
| 12  | 2.000 | 2.4 | 0.35 | 31.7 |
| 13  | 2.000 | 2.0 | 0.33 | 34.8 |
| 14  | 2.000 | 2.6 | 0.36 | 38.9 |
| 15  | 2.000 | 2.4 | 0.35 | 36.8 |
| CE1 | 2.000 | 1.4 | 0.35 | 12.4 |
| CE2 | 2.000 | 1.6 | 0.32 | 22.6 |
| CE3 | 2.000 | 1.2 | 0.28 | 8.2  |
| CE4 | 2.000 | 2.2 | 0.32 | 18.1 |
| CE5 | 1.500 | 2.9 | 0.32 | 7.8  |
| CE6 | 1.000 | 3.6 | 0.31 | 2.7  |
| CE7 | 2.000 | 1.1 | 0.22 | 7.8  |

\* CE : Comparative Examples

As shown above, the production process of the catalyst of the present invention for homo-polymerization and co-polymerization of ethylene is simple with excellent catalytic activity. Further, with the catalyst particles being controlled, high bulk density of the polymer can be provided, and the hydrogen sensitivity is greatly improved..

### ABSTRACT

5 The present invention relates to a catalyst for homo-polymerization or co-polymerization of  
ethylene, or more particularly to a solid complex titanium catalyst for homo-polymerization or  
co-polymerization of ethylene. ~~said The catalyst being may be produced by preparing a~~  
magnesium solution by contact-reacting a ~~halogenated magnesium~~ magnesium halide compound  
with alcohol. ~~rReacting said the~~ solution with an ester compoound having at least one hydroxy  
group and a silicon compound having an alkoxy group, ~~and tThen reacting said the~~ solution  
10 with a mixture of a titanium compound and a silicon compound. ~~The catalyst of the present~~  
invention has high activity with superior hydrogen sensitivity.

A CATALYST FOR ETHYLENE HOMO- AND CO-POLYMERIZATIONTechnical Field

5 The present invention relates to a catalyst for homo-polymerization or co-polymerization of ethylene, or more particularly to a high-activity titanium solid complex catalyst supported in a carrier containing magnesium, said catalyst showing high catalytic activity, high bulk density, and high hydrogen sensitivity.

Background of the Invention

10 Catalysts containing magnesium for polymerization or co-polymerization of ethylene are known to have very high catalytic activities and to accord good bulk density, which are in turn suitable for liquid phase or gas phase polymerization. By liquid phase polymerization of ethylene, it denotes the polymerization process performed in such medium of bulk ethylene, isopentane, or hexane, and as for the important characteristics in consideration of the applicability of the catalyst used in this process, they are as follows: high activity, bulk density, 15 the amount of molecules of low molecular weight dissolved in a medium, etc. Furthermore, in most of these manufacturing processes, hydrogen is used to control the molecular weight. The changes in the molecular weight (hereinafter hydrogen sensitivity) according to the amount of hydrogen is another characteristic of a catalyst, which is different per catalyst. The catalyst with high hydrogen sensitivity can control the molecular weight by using less amount of hydrogen at 20 the time of the application of the process. As such, it provides more leeway with respect to the operation of the process.

25 Many of the titanium-based catalysts containing magnesium for olefin polymerization, and the manufacturing methods thereof have been reported. Especially, many processes making use of magnesium solutions to obtain olefin polymerization catalysts of good bulk density have been known. There is a means of obtaining a magnesium solution by reacting magnesium compounds with such electron donors as alcohol, amine, cyclic ether, or organic carboxylic acid in the presence of a hydrocarbon solvent. As for the cases of use of alcohol, they are disclosed 30 in US Patent Nos. 4,330,649, and 5,106,807. Further, the methods for production of catalysts containing magnesium by reacting a liquid magnesium solution with a halogenated compound

such as titanium tetrachloride are well known. Such catalysts provide good bulk density, but there is much yet to be improved with respect to their catalytic activities and hydrogen sensitivity. In US Patent Nos. 4,477,639 and 4,518,706, a cyclic ether, tetrahydrofuran was used as a solvent of the magnesium compound.

US Patent Nos. 4,847,227, 4,816,433, 4,829,037, 4,970,186, and 5,130,284 claimed the methods of producing olefin polymerization catalysts of good bulk density, with superior polymerization activity due to the reaction of a titanium chloride compound with an electron donor compound such as magnesium alkoxide, dialkyl phthalate, and phthaloyl chloride.

US Patent No. 5,459,116 reports the method of producing supported titanium solid catalysts by means of contact-reacting a titanium compound and a magnesium solution containing an ester having at least one hydroxy group as an electron donor. By using this method, it is possible to obtain a catalyst of superior polymerization activity and bulk density. However, there remain things to be improved with respect to hydrogen sensitivity.

US Patent No. 5,869,418 shows the method of increasing hydrogen sensitivity by using a dialkoxyphenylalkane in the propylene polymerization as an external electron donor, and the advantages of such method. However, the above effects were obtained by using the external electron donor in addition to the solid catalyst, and also it is limited to polymerization and co-polymerization of propylene.

#### Summary of the Invention

As shown above, there is a need for the development of a new catalyst for homopolymerization or co-polymerization of ethylene for producing polymers with the following conditions: simple manufacturing process, high polymerization activity, high bulk density for polymers by means of controlling the catalyst particles, and high hydrogen sensitivity. In the present invention, therefore, it is intended to provide a method for producing, from low-cost compounds via a simple process, a catalyst having an excellent catalytic activity, and superior hydrogen sensitivity, capable of producing polymers of good bulk density. Further, the specific production process of catalysts and the steps thereof as disclosed in the present invention have never been reported in the prior art.

Consequently, the objective of the present invention is to provide a new catalyst solid component for homo-polymerization or co-polymerization of ethylene, said catalyst having superior catalytic activity and hydrogen sensitivity, capable of producing polymers of high bulk density. More specifically, the objective of the present invention lies in providing a catalyst solid component for homo-polymerization or co-polymerization of ethylene, having a superior hydrogen sensitivity, wherein the form of the catalyst particles are controlled therein.

Another objective of the present invention is to provide a simple process for producing a catalyst for homo-polymerization or co-polymerization of ethylene.

Still other objectives and the utility of the present invention will become apparent as references are made with respect to the following descriptions and the claims thereto.

#### Detailed Description of the Preferred Embodiments

The catalyst of superior catalytic activity and hydrogen sensitivity, capable of producing polymers having high bulk density as provided in the present invention, is produced by a simple yet efficient manufacturing process, which comprises (i) preparing a magnesium solution by contact-reacting a halogenated magnesium compound, with an alcohol, (ii) reacting the same with an ester compound containing at least one hydroxy group and a silicon compound containing an alkoxy group, and (iii) producing a solid titanium catalyst by adding a titanium compound and a silicon compound.

Types of halogenated magnesium compounds used in the present invention are as follows: di-halogenated magnesiums such as magnesium chloride, magnesium iodide, magnesium fluoride, and magnesium bromide; alkylmagnesium halides such as methylmagnesium halide, ethylmagnesium halide, propylmagnesium halide, butylmagnesium halide, isobutylmagnesium halide, hexylmagnesium halide, amylmagnesium halide; alkoxymagnesium halides such as methoxymagnesium halide, ethoxymagnesium halide, isopropoxymagnesium halide, butoxymagnesium halide, octoxymagnesium halide; and aryloxymagnesium halides such as phenoxymagnesium halide and methyl-phenoxymagnesium halide. Of the above magnesium compounds, two or more compounds can be used in a mixture. Further, the above magnesium compounds can be effectively used in the form of a complex compound with other metals.

Of the compounds listed above, some can be represented by a simple formula, but the others cannot be so represented depending on the production methods of magnesium compounds. In the latter cases, it can be generally regarded as a mixture of some of the listed compounds.

5 For example, the following compounds can be used in the present invention: such compounds obtained by reacting magnesium compounds with polysilolxane compounds, silane compounds containing halogen, ester, or alcohol; and such compounds obtained by reacting magnesium metals with alcohol, phenol, or ether in the presence of halosilane, phosphorus pentachloride, or thionyl chloride. However, the preferable magnesium compounds are magnesium halides,  
10 especially magnesium chloride or alkylmagnesium chloride, preferably those having an alkyl group of 1 ~ 10 carbons; alkoxymagnesium chlorides, preferably those having 1 ~ 10 carbons; and aryloxymagnesium chlorides, preferably those having 6 ~ 20 carbons. The magnesium solution used in the present invention is made by dissolving the aforementioned compounds with alcohol as a solvent in the presence or absence of a hydrocarbon solvent.

15 As to the types of hydrocarbon solvents used in the present invention, they include aliphatic hydrocarbons such as pentane, hexane, heptane, octane, decane, and kerosene; alicyclic hydrocarbons such as cyclohexane, methylcyclohexane, cyclohexane, and methylcyclohexane; aromatic hydrocarbons such as benzene, toluene, xylene, ethylbenzene, cumene, and cymene;  
20 and halogenated hydrocarbons such as dichloropropane, dichloroethylene, trichloroethylene, carbon tetrachloride, and chlorobenzene.

When a magnesium compound is converted into a magnesium solution, alcohol is used in the presence or absence of the aforementioned hydrocarbons. The types of alcohol include  
25 those containing 1 ~ 20 carbon atoms such as methanol, ethanol, propanol, butanol, pentanol, hexanol, octanol, decanol, dodecanol, octadecyl alcohol, benzyl alcohol, phenylethyl alcohol, isopropyl benzyl alcohol, and cumyl-alcohol, although alcohols containing 1 ~ 12 carbon atoms are preferable. The average size of a target catalyst and its particle distribution can vary according to the type of alcohol, the total contents, types of magnesium compounds, and the ratio  
30 of magnesium to alcohol, etc. Nevertheless, the total amount of alcohol required to obtain the magnesium solution is at least 0.5 mol per each mole of the magnesium compound, preferably about 1.0 ~ 20 mol, or more preferably about 2.0 ~ 10 mol.

The reaction of a magnesium compound with alcohol for producing magnesium solution is preferably carried out in the presence of hydrocarbon. The reaction temperature, while variable depending on the type and the amount of alcohol, is at least -25°C, preferably -10 ~ 200°C, or more preferably about 0 ~ 150°C. It is preferable to carry out the reaction for about 15 minutes ~ 5 hours, preferably for about 30 minutes ~ 4 hours.

Of the electron donors used in the present invention, the ester compounds containing at least one hydroxy group include unsaturated aliphatic acid esters having at least one hydroxy group such as, 2-hydroxy ethylacrylate, 2-hydroxy ethylmethacrylate, 2-hydroxypropyl acrylate, 2-hydroxypropylmethacrylate, 4-hydroxy butylacrylate, pentaerythritol triacrylate; aliphatic monoesters or polyesters containing at least one hydroxy group such as 2-hydroxy ethyl acetate, methyl 3-hydroxy butylate, ethyl 3-hydroxy butylate, methyl 2-hydroxy isobutylate, ethyl 2-hydroxy isobutylate, methyl 3-hydroxy-2-methyl propionate, 2,2-dimethyl-hydroxy propionate, ethyl-6-hydroxy hexanoate, t-butyl-2-hydroxy isobutylate, diethyl-3-hydroxy glutarate, ethyl lactate, isopropyl lactate, butyl isobutyl lactate, isobutyl lactate, ethyl mandelate, dimethyl ethyl tartrate, ethyl tartrate, dibutyl tartrate, diethyl citrate, triethyl citrate, ethyl-2-hydroxy-caproate, diethyl bis-(hydroxy methyl)malonate; aromatic esters having at least one hydroxy group such as 2-hydroxy ethyl benzoate, 2-hydroxy ethyl salicylate, methyl-4-(hydroxy methyl) benzoate, methyl-4-hydroxy benzoate, ethyl-3-hydroxy benzoate, 4-methyl salicylate, ethyl salicylate, phenyl salicylate, propyl-4-hydroxy benzoate, phenyl-3-hydroxy naphthanoate, monoethylene glycol monobenzoate, diethylene glycol benzoate, triethylene glycol benzoate; alicyclic esters having at least one hydroxy group such as lactone, and others. The amount of the ester compound containing at least one hydroxy group should be 0.001 ~ 5 mol per mole of magnesium, or preferably 0.01 ~ 2 mol per mole of magnesium.

For the silicon compound containing an alkoxy group, the other electron donor in the present invention, a compound having a general formula of  $R^1_nSi(OR^2)_{4-n}$  (here,  $R^1$  and  $R^2$  represents a hydrocarbon having 1 ~ 12 carbons, and  $n$  for an integer of 0 ~ 3) is preferable. More specifically, it includes dimethyldimethoxy silane, dimethyldiethoxy silane, diphenyldimethoxy silane, methylphenyldimethoxy silane, diphenyldiethoxy silane, ethyltrimethoxy silane, vinyltrimethoxy silane, methyltrimethoxy silane, phenyltrimethoxy

silane, methyltriethoxy silane, ethyltriethoxy silane, vinyltriethoxy silane, butyltriethoxy silane, phenyltriethoxy silane, ethyltriisopropoxy silane, vinyltributoxy silane, ethyl silicate, butyl silicate, methyltriaryloxy silane, etc. The amount of such compound should be 0.05 ~ 3 mol per mole of magnesium, or more preferably 0.1 ~ 2 mol per mole of magnesium.

5

As for the temperature for the contact-reaction of a magnesium solution, an ester compound containing at least one hydroxy group, and an alkoxy silicon compound, the temperature of 0 ~ 100°C is appropriate, or more preferably 10 ~ 70°C.

10

In the process, the catalyst particles are recrystallized by reacting the magnesium compound solution with a mixture of a liquid titanium compound of a general formula of  $\text{Ti}(\text{OR})_a\text{X}_{4-a}$  (R-stands for an alkyl group with 1 ~ 10 carbons; X for a halogen atom; and "a" for a natural number of 0 to 4) and a silicon compound of a general formula of  $\text{R}_n\text{SiCl}_{4-n}$  (here R stands for hydrogen; or an alkyl, alkoxy, haloalkyl, or aryl group having 1 to 10 carbons; or a halosilyl or halosilyl alkyl group having 1 to 8 carbons;  $n = 0-3$ ). The types of titanium compounds which satisfy the general formula of  $\text{Ti}(\text{OR})_a\text{X}_{4-a}$  include 4-halogenated titanium such as  $\text{TiCl}_4$ ,  $\text{TiBr}_4$ , and  $\text{TiI}_4$ ; 3-halogenated alkoxy-titanium such as  $\text{Ti}(\text{OCH}_3)\text{Cl}_3$ ,  $\text{Ti}(\text{OC}_2\text{H}_5)\text{Cl}_3$ ,  $\text{Ti}(\text{OC}_2\text{H}_5)\text{Br}_3$ , and  $\text{Ti}(\text{O}(\text{i-C}_4\text{H}_9))\text{Br}_3$ ; 2-halogenated alkoxy-titanium compounds such as  $\text{Ti}(\text{OCH}_3)_2\text{Cl}_2$ ,  $\text{Ti}(\text{OC}_2\text{H}_5)_2\text{Cl}_2$ ,  $\text{Ti}(\text{O}(\text{i-C}_4\text{H}_9))_2\text{Cl}_2$ , and  $\text{Ti}(\text{OC}_2\text{H}_5)_2\text{Br}_2$ ; and tetra-alkoxy titaniums such as  $\text{Ti}(\text{OCH}_3)_4$ ,  $\text{Ti}(\text{OC}_2\text{H}_5)_4$ , and  $\text{Ti}(\text{OC}_4\text{H}_9)_4$ . A mixture of the above titanium compounds can also be used in the present invention. However, the preferable titanium compounds are those containing halogen, or more preferably titanium tetrachloride.

15

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The types of silicon compounds satisfying the above general formula of  $\text{R}_n\text{SiCl}_{4-n}$  include silicon tetrachloride; trichlorosilanes such as trichlorosilane, methyltrichlorosilane, ethyltrichlorosilane, phenyltrichlorosilane; dichlorosilanes such as dimethylchlorosilane, diethyldichlorosilane, di-phenyldichlorosilane, and methylphenyldichlorosilane; monochlorosilanes such as trimethylchlorosilane; and a mixture of these silicon compounds can also be used in the present invention, or more preferably silicon tetrachloride can be used.

30

The amount of the mixture of a titanium compound and a silicon compound used during the re-crystallization of the magnesium compound solution is appropriately 0.1 ~ 200 mol per

mole of the halogenated magnesium compound, preferably 0.1 ~ 100 mol, or more preferably 0.2 ~ 80 mol. The molar ratio of a titanium compound to a silicon compound in the mixture is appropriately 0.05 ~ 0.95, or more preferably 0.1 ~ 0.8. When the magnesium compound solution is reacted with the mixture of a titanium compound and a silicon compound, the shape and the size of the resultant re-crystallized solid constituents vary a great deal according to the reaction conditions. In order to obtain the target size of the catalyst and the size and distribution of the polymers, as intended by the present invention, it is advantageous to maintain the above mixture amounts for said titanium and silicon compounds, as well as their mix ratios. If it is outside of the above range, it will be difficult to obtain the results as intended. The reaction of the magnesium compound with the mixture of a titanium compound and a silicon compound should be carried out preferably at a sufficiently low temperature to result in formation of solid constituents. More preferably, the reaction should be carried out by contact-reaction at -70 ~ 70°C, or most preferably at -50 ~ 50°C. After the contact-reaction the reacting temperature is slowly raised for sufficient reaction for the duration of 0.5 ~ 5 hours at 50 ~ 150°C.

The particles of the solid catalysts obtained during the above process can be further reacted with titanium compounds. These titanium compounds are titanium halides, and halogenated alkoxy titanium with an alkoxy functional group of 1 ~ 20 carbons. At times, a mixture of these compounds can also be used. Of these compounds, however, titanium halide and a halogenated alkoxy titanium compound having an alkoxy functional group of 1~8 carbons can be appropriately used, or more preferably titanium tetrahalide can be used.

Further, the solid complex titanium catalysts produced during the process of the present invention can be utilized during homo-polymerization or co-polymerization of ethylene. In particular, the catalyst is used in homo-polymerization of ethylene, and also in co-polymerization of ethylene and  $\alpha$  -olefin such as propylene, 1-butene, 1-pentene, 1-methyl-1-pentene, or 1-hexene having three or more carbons.

The polymerization reaction in the presence of the catalyst of the present invention is carried out by means of using (i) a solid complex titanium catalyst of the present invention, comprising magnesium, titanium, halogen, and electron donors, and (ii) a cocatalyst comprising, compounds of organic metals of Groups II and III of the Periodic Table.

The solid complex titanium catalyst constituents of the present invention can be used in pre-polymerization of ethylene or  $\alpha$ -olefin prior to the use in the aforementioned polymerization reaction. The pre-polymerization can be carried out in the presence of a hydrocarbon solvent such as hexane, at a sufficiently low temperature, with ethylene or  $\alpha$ -olefin under pressure, in the presence of the above catalyst constituents and such an organic aluminum compound as triethylaluminum. Pre-polymerization, by maintaining the shape of the catalyst by surrounding the catalyst particles with polymers, is helpful in producing food-quality post-polymerization shape of the polymers. The weight ratio of the polymers to the catalysts after pre-polymerization is ordinarily 0.1 : 1 to 20 : 1.

The organometallic compound in the present invention can be represented by a general formula of  $MR_n$ , wherein, M stands for a metal constituent of Group II or IIIA in the Periodic Table, such as magnesium, calcium, zinc, boron, aluminum, and gallium, R for an alkyl group with 1 ~ 20 carbons, such as a methyl, ethyl, butyl, hexyl, octyl, or decyl group, and n for the atomic value of the metal constituent. As for more preferable organometallic compounds, trialkyl aluminum having an alkyl group of 1 ~ 6 carbons, such as triethylaluminum and triisobutylaluminum, or the mixture thereof can be utilized. On occasions, an organic aluminum compound having one or more halogen or hydride groups, such as ethylaluminum dichloride, diethylaluminum chloride, ethyl-aluminum sesqui-chloride, or diisobutylaluminum hydride can also be used.

As for the polymerization reaction, it is possible to carry out either gas phase or bulk polymerization in the absence of an organic solvent, or liquid slurry polymerization in the presence of an organic solvent. These polymerization methods, however, are carried out in the absence of oxygen, water, or other compounds that may act as catalytic poison.

The concentration of the solid complex titanium compound (i) with respect to the polymerization system, in the case of a liquid phase slurry polymerization, is approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the solvent, or more preferably approximately 0.001 ~ 0.5 mmol. As for the solvent, the following compounds or the mixtures thereof can be used: alkanes or cycloalkanes such as pentane, hexane, heptane, n-

octane, isooctane, cyclohexane, methylcyclohexane; alkylaromatic such as toluene, xylene, ethylbenzene, isopropylbenzene, ethyltoluene, n-propylbenzene, diethylbenzene; and halogenated aromatics such as chlorobenzene, chloronaphthalene, ortho-dichlorobenzene.

5 In the case of gas phase polymerization, the amount of the solid complex titanium catalyst (i) should be approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the polymerization reactant, preferably approximately 0.001 ~ 1.0 mmol, or more preferably approximately 0.01 ~ 0.5 mmol.

10 The preferable concentration of the organometallic compound (ii) is about 1 - 2,000 mol, as calculated by the aluminum atoms, per mole of the titanium atoms in the catalyst (i), or more preferably about 5 ~ 500 mol.

15 To secure a high reaction rate of polymerization, the polymerization herein is carried out at a sufficiently high temperature, regardless of the polymerization manufacturing process. Generally, the temperature of approximately 20 ~ 200°C is appropriate, or more preferably approximately 20 ~ 95°C. The appropriate pressure of monomers at the time of polymerization is the atmospheric to 100 atm, or more preferably 2 ~ 50 atm.

20 In the present invention, in order to evaluate the hydrogen reactivity of the catalyst, the changes in the molecular weight according to the amount of hydrogen at the time of polymerization are shown as a melt index (ASTM D 1238), the index generally known in the art. The value of the melt index generally becomes greater as the molecular weight decreases.

25 The products obtained by the method of polymerization of the present invention are solid ethylene homogeneous polymers or the copolymers of ethylene and  $\alpha$ -olefin, which have excellent bulk density and fluidity. Since the polymer yields are sufficiently high, there is no need for the removal of the catalyst residues.

30 The present invention is further described by means of the examples and comparative examples as below but should not be confined or limited to these examples.

## Example 1

### Production of catalyst

A solid complex titanium catalyst was produced by means of the following three steps:

#### (i) Step: Production of magnesium solution

Into a 1.0L reactor equipped with a mechanical stirrer, replaced with nitrogen atmosphere, 9.5 g of  $\text{MgCl}_2$  and 400 ml of decane were placed therein. After they were stirred at 300 rpm, 60 ml of 2-ethyl hexanol was added thereto. The temperature was raised to 120 °C, and then the reaction was allowed to continue for three hours. The homogenous solution, which was obtained after the reaction, was cooled to room temperature (25°C).

#### (ii) Step : Contact-reaction of a magnesium solution, an ester containing a hydroxy group and an alkoxy boron compound

To the magnesium solution, cooled to room temperature as above, 1.2 ml of 2-hydroxyethyl methacrylate and 10 ml (45 mmol) of silicon tetraethoxide were added, and then the reaction was allowed to continue for an hour.

#### (iii) Step : Treatment of a mixture of a titanium compound and a silicon compound

After cooling the above solution to room temperature (25°C), a solution mixture of 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride was dripped into the above solution for one hour. After the completion of the dripping process, the temperature of the reactor was raised to 90°C while stirring, after which was maintained at that temperature for one hour. After stopping the stirring, the supernatant of the solution was removed, and to the remaining solid layer was added 300 ml of decane and 100 ml of titanium tetrachloride in sequence. There, the temperature was raised to 100°C and

maintained thereat for two hours. After the reaction, the reactor was cooled to room temperature and the washing of the resulting solid product with 400ml of hexane was repeated until the removal of free unreacted titanium chloride. The titanium content of the solid catalyst so produced was 3.6%.

### Polymerization

A 2-L high-pressure reactor was dried in an oven and assembled while still hot. In order to make the inside of the reactor nitrogen atmosphere, nitrogen and vacuum were alternatively manipulated three times in the reactor. To the reactor was added 1,000 ml of n-hexane, after which 2 mmols of triethylaluminum and a solid catalyst by 0.03 mmol in terms of the titanium atoms were added thereto. Then, 2000 ml of hydrogen was added. The temperature was raised to 80°C while stirring at 700 rpm. The pressure of ethylene was adjusted to 80 psi, and the polymerization was allowed to continue for an hour. After the polymerization, the temperature of the reactor was lowered to room temperature, and a large amount of ethanol was added to stop the polymerization. The polymer thus produced was collected by separation and was dried in an oven at 50°C for at least six hours, whereby polyethylene was obtained in the form of white powder.

The polymerization activity (kg of polyethylene divided by mmol of Ti) was calculated as the weight (kg) ratio of the polymer as produced per the amount of the catalysts so used (mmol of Ti). The results of the polymerization are shown in Table 1, together with the bulk density (g/ ml) of the polymers and the melt index (g/10 minutes).

### Example 2

The catalyst was prepared the same as in Example 1, except that in Step (ii) of Example 1, the temperature of the magnesium solution was adjusted to room temperature (25°C). The titanium content of the catalyst thus produced was 3.2 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

### Example 3

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 2.4 ml of 2-hydroxyethyl methacrylate and 10.0 ml of silicon tetraethoxide were used. The titanium content of the catalyst thus produced was 2.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 4

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 3.6 ml of 2-hydroxyethyl methacrylate and 10.0 ml of silicon tetraethoxide were used. The titanium content of the catalyst thus produced was 2.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 5

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 1.2 ml of 2-hydroxyethyl methacrylate and 5.0 ml of silicon tetraethoxide were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 6

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 1.2 ml of 2-hydroxyethyl methacrylate and 15.0 ml of silicon tetraethoxide were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.1 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 7

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride were dripped in the period of 30 minutes for production of the catalyst. The titanium content of the catalyst thus produced

was 3.8 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 8

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride were dripped in the period of 2 hours for production of the catalyst. The titanium content of the catalyst thus produced was 3.6 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 9

The polymerization was carried out using the catalyst produced in Example 1 and 1500 ml of hydrogen, and the results thereof are shown in Table 1.

#### Example 10

The polymerization was carried out using the catalyst produced in Example 1 and 1000 ml of hydrogen, and the results thereof are shown in Table 1.

#### Example 11

The catalyst was prepared the same as in Example 2, except that in Step (i) of Example 2, 400 ml of decane was used in the production of magnesium solution. The titanium content of the catalyst thus produced was 3.6 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 12

The catalyst was prepared the same as in Example 11, except that in Step (iii) of Example 11, 40 ml of titanium tetrachloride and 20 ml of silicon tetrachloride were used. The titanium

content of the catalyst thus produced was 3.8 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 13

The catalyst was prepared the same as in Example 12, except that in Step (iii) of Example 12, 20 ml of titanium tetrachloride and 40 ml of silicon tetrachloride were used. The titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 14

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 40 ml of titanium tetrachloride and 20 ml of silicon tetrachloride were used. The titanium content of the catalyst thus produced was 3.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 15

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 20 ml of titanium tetrachloride and 40 ml of silicon tetrachloride were used. The titanium content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Comparative Example 1

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 10.0 ml of silicon tetraethoxide was added and 2-hydroxyethyl methacrylate was not used. The titanium content of the catalyst thus produced was 3.8 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

### Comparative Example 2

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, 1.2 ml of 2-hydroxyethyl methacrylate was added and silicon tetraethoxide was not used. The titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

### Comparative Example 3

The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, neither 2-hydroxyethyl methacrylate nor silicon tetraethoxide was used. The titanium content of the catalyst thus produced was 4.3 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

### Comparative Example 4

The catalyst was prepared the same as in Example 2, except that in Step (iii) of Example 2, 60 ml of titanium tetrachloride was used. The titanium content of the catalyst thus produced was 4.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

### Comparative Example 5

The polymerization was carried out using the catalyst produced in Comparative Example 4 and 1500 ml of hydrogen. The results thereof are shown in Table 1.

### Comparative Example 6

The polymerization was carried out using the catalyst produced in Comparative Example 4 and 1000 ml of hydrogen. The results thereof are shown in Table 1.

### Comparative Example 7

5 The catalyst was prepared the same as in Example 2, except that in Step (ii) of Example 2, neither 2-hydroxyethyl methacrylate nor silicon tetraethoxide was used, and in Step (iii) 60 ml of titanium tetrachloride was used. The titanium content of the catalyst thus produced was 4.1 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Table 1 Results of Polymerization

| Example | Amount of Hydrogen (ml) | Activity (kg PE/mmol Ti) | Bulk Density (g/ml) | Melting Index (g/10min) |
|---------|-------------------------|--------------------------|---------------------|-------------------------|
| 1       | 2.000                   | 2.3                      | 0.36                | 38.9                    |
| 2       | 2.000                   | 2.1                      | 0.35                | 35.2                    |
| 3       | 2.000                   | 2.5                      | 0.34                | 38.4                    |
| 4       | 2.000                   | 2.3                      | 0.33                | 39.2                    |
| 5       | 2.000                   | 2.6                      | 0.34                | 33.1                    |
| 6       | 2.000                   | 2.0                      | 0.36                | 32.4                    |
| 7       | 2.000                   | 2.7                      | 0.32                | 38.1                    |
| 8       | 2.000                   | 2.1                      | 0.35                | 34.8                    |
| 9       | 1.500                   | 2.8                      | 0.34                | 19.8                    |
| 10      | 1.000                   | 3.9                      | 0.32                | 3.8                     |
| 11      | 2.000                   | 2.2                      | 0.34                | 36.4                    |
| 12      | 2.000                   | 2.4                      | 0.35                | 31.7                    |
| 13      | 2.000                   | 2.0                      | 0.33                | 34.8                    |
| 14      | 2.000                   | 2.6                      | 0.36                | 38.9                    |
| 15      | 2.000                   | 2.4                      | 0.35                | 36.8                    |
| CE1     | 2.000                   | 1.4                      | 0.35                | 12.4                    |
| CE2     | 2.000                   | 1.6                      | 0.32                | 22.6                    |
| CE3     | 2.000                   | 1.2                      | 0.28                | 8.2                     |
| CE4     | 2.000                   | 2.2                      | 0.32                | 18.1                    |
| CE5     | 1.500                   | 2.9                      | 0.32                | 7.8                     |
| CE6     | 1.000                   | 3.6                      | 0.31                | 2.7                     |
| CE7     | 2.000                   | 1.1                      | 0.22                | 7.8                     |

\* CE : Comparative Examples

10 As shown above, the production process of the catalyst of the present invention for homo-polymerization and co-polymerization of ethylene is simple with excellent catalytic activity. Further, with the catalyst particles being controlled, high bulk density of the polymer can be provided, and the hydrogen sensitivity is greatly improved..

## Claims

What is claimed is:

- 5 1. A solid titanium catalyst for homo-polymerization and co-polymerization of ethylene, wherein said catalyst is produced by:
  - (i) preparing a magnesium compound solution by contacting a halogenated magnesium compound with alcohol;
  - 10 (ii) reacting said solution with an ester compound having at least one hydroxy group and a silicon compound having an alkoxy group; and
  - (iii) reacting the solution from above(ii) with a mixture of a titanium compound and a silicon compound to produce solid catalyst, and optionally the solid catalyst are further reacted with a titanium compound.
2. A solid titanium catalyst according to Claim 1, wherein said ester compound having at least one hydroxy group is an unsaturated aliphatic ester having at least one hydroxy group, which is selected from the group consisting of 2-hydroxy ethylacrylate, 2-hydroxy ethylmethacrylate, 2-hydroxy propyl acrylate, 2-hydroxy propylmethacrylate, 4-hydroxy butylacrylate, pentaerithritol triacrylate; an aliphatic monoester or polyester having at least one hydroxy group, which is selected from the group consisting of 2-hydroxy ethyl acetate, methyl 3-hydroxy butylate, ethyl 3-hydroxy butylate, methyl 2-hydroxy isobutylate, ethyl 2-hydroxy isobutylate, methyl 3-hydroxy-2-methyl propionate, 2,2-dimethyl-3-hydroxy propionate, ethyl-6-hydroxy hexanoate, t-butyl-2-hydroxy isobutylate, diethyl-3-hydroxy glutarate, ethyllactate, isopropyl lactate, butyl-isobutyl lactate, isobutyl lactate, ethyl mandelate, dimethyl ethyl tartrate, ethyl tartrate, dibutyl tartrate, diethyl citrate, triethyl citrate, ethyl-2-hydroxy-caproate, diethyl *bis*-(hydroxymethyl malonate; an aromatic ester having at least one hydroxy group, which is selected from the group consisting of 2-hydroxy ethyl benzoate, 2-hydroxy ethyl salicylate, methyl-4-(hydroxy methyl) benzoate, methyl-4-hydroxy benzoate, ethyl-3-hydroxy benzoate, 4-methyl salicylate, ethyl salicylate, phenyl salicylate, propy-4-hydroxy benzoate, phenyl-3-hydroxy naphthanoate, monoethylene glycol monobenzoate, diethylene glycol benzoate, triethylene glycol monobenzoate; an alicyclic ester having at least one hydroxy group as in hydroxy butyl-lactone; and wherein said silicon

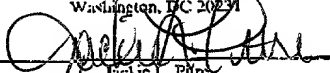
compound having an alkoxy group is represented by the general formula of  $R^1_nSi(OR^2)_{4-n}$ , wherein  $R^1$  and  $R^2$  represent a hydrocarbon having 1 ~ 12 carbons, and n for an integer of 0 ~ 3, said silicon compound being selected from the group consisting of dimethyldimethoxy silane, dimethyldiethoxy silane, diphenyldimethoxy silane, methylphenyldimethoxy silane, diphenyldiethoxy silane, ethyltrimethoxy silane, vinyltrimethoxy silane, methyltrimethoxy silane, phenyltrimethoxy silane, methyltriethoxy silane, ethyltriethoxy silane, vinyltriethoxy silane, butyltriethoxy silane, phenyltriethoxy silane, ethyltriisopropoxy silane, vinyltributoxy silane, ethylsilicate, butylsilicate, and methyltriaryloxy silane.

3. A solid titanium catalyst according to Claim 1, wherein said titanium compound is represented by the general formula of  $Ti(OR)_aX_{4-a}$ , where R stands for an alkyl group with 1 ~ 20 carbons, X for a halogen atom, and "a" for an integer of 0 to 4; and wherein said silicon is represented by the general formula of  $R_nSiCl_{4-n}$ , where R stands for hydrogen, or an alkyl, alkoxy, haloalkyl, or aryl group having 1 to 10 carbons; a halosilyl or halosilyl alkyl group having 1 to 8 carbons; n = an integer of 0 to 4.
4. A solid titanium catalyst according to Claim 3, wherein said titanium compound is a 4-halogenated titanium, which is selected from the group consisting of  $TiCl_4$ ,  $TiBr_4$ , and  $TiI_4$ ; a 3-halogenated alkoxy titanium, which is selected from the group consisting of  $Ti(OCH_3)Cl_3$ ,  $Ti(OC_2H_5)Cl_3$ ,  $Ti(OC_2H_5)Br_3$ , and  $Ti(O(i-C_4H_9))Br_3$ ; a 2-halogenated alkoxy titanium, which is selected from the group consisting of  $Ti(OCH_3)_2Cl_2$ ,  $Ti(OC_2H_5)_2Cl_2$ ,  $Ti(O(i-C_4H_9))_2Cl_2$ , and  $Ti(OC_2H_5)_2Br_2$ ; and a tetralkoxy titanium, which is selected from the group consisting of  $Ti(OCH_3)_4$ ,  $Ti(OC_2H_5)_4$ , and  $Ti(OC_4H_9)_4$ ; and wherein said silicon compound is a silicon tetrachloride; a trichlorosilane such as methyltrichlorosilane, ethyltrichlorosilane, and phenyl-trichlorosilane; a dichlorosilane such as dimethylchlorosilane, diethyldichlorosilane, diphenyldichlorosilane, and methylphenyldichlorosilane; and a monochlorosilane such as trimethylchlorosilane.
5. The solid titanium catalyst according to Claim 3, wherein said titanium compound comprises titanium tetrachloride, and said silicon compound comprises silicon tetrachloride.

## ABSTRACT

5       The present invention relates to a catalyst for homo-polymerization or co-polymerization of  
ethylene, or more particularly to a solid complex titanium catalyst for homo-polymerization or  
co-polymerization of ethylene, said catalyst being produced by preparing a magnesium solution  
by contact-reacting a halogenated magnesium compound with alcohol, reacting said solution  
with an ester compound having at least one hydroxy group and a silicon compound having an  
10 alkoxy group, and then reacting said solution with a mixture of a titanium compound and a  
silicon compound. The catalyst of the present invention has high activity with superior hydrogen  
sensitivity.

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Sir:

The undersigned, being Assignee of record of the entire interest in the above-identified application by virtue of an assignment recorded in the United States Patent and Trademark Office as set forth below, hereby elects, under 37 C.F.R. § 3.71, to prosecute the application to the exclusion of the inventors.

The Assignee hereby revokes any previous Powers of Attorney and appoints:

|                       |                        |
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| B. Noel Kivlin        | Reg. No. <u>33,929</u> |
| Robert C. Kowert      | Reg. No. <u>39,255</u> |
| Mark Lupkowski        | Reg. No. <u>49,010</u> |

Chun ByungYang  
09/980,168

|                    |                        |
|--------------------|------------------------|
| Lawrence J. Merkel | Reg. No. 41,191        |
| Eric B. Meyertons  | Reg. No. <u>34,876</u> |
| Louise K. Miller   | Reg. No. <u>36,609</u> |
| Theresa Moorman    | Reg. No. <u>46,941</u> |
| David W. Quimby    | Reg. No. <u>39,338</u> |
| Rory D. Rankin     | Reg. No. <u>47,884</u> |
| David A. Rose      | Reg. No. <u>26,223</u> |
| Doug Shamah        | Reg. No. <u>45,093</u> |

each an attorney or agent of the firm of CONLEY, ROSE & TAYON, P.C., as its attorney or agent for so long as they remain with such firm, with full power of substitution and revocation, to prosecute the application, to make alterations and amendments therein, to transact all business in the Patent and Trademark Office in connection therewith, and to receive any Letters Patent, and for one year after issuance of such Letters Patent to file any request for a certificate of correction that may be deemed appropriate.

Pursuant to 37 C.F.R. § 3.73, the undersigned has reviewed the evidentiary documents, specifically the Assignment to Samsung General Chemicals Co., Ltd., referenced below, and certify that to the best of my knowledge and belief, title remains in the name of the Assignee.

Please direct all communications as follows:

Eric B. Meyertons, Esq.  
CONLEY, ROSE & TAYON, P.C.  
P.O. BOX 398  
AUSTIN, TEXAS 78767-0398  
(512) 476-1400 (voice)  
(512) 703-1250 (facsimile)

ASSIGNEE:

SAMSUNG GENERAL CHEMICALS CO.,  
LTD.

By:  

Title:

Date: March 25, 2002

ASSIGNMENT: X Enclosed for recording

PATENT  
5333-02500**DECLARATION**

As a below named inventor, I hereby declare that:

My residence, post office and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or the below named inventors believe they are the original, first and joint inventors (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled **A CATALYST FOR ETHYLENE HOMO- AND CO-POLYMERIZATION**, the specification of which:

☐ is attached herewith.☒ was filed on November 27, 2001 as Application Serial No. 09/980,168.

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose to the Patent and Trademark Office all information known to me to be material to patentability of the subject matter claimed in this application, as "materiality" is defined in Title 37, Code of Federal Regulations, § 1.56.

I hereby claim foreign priority benefits under Title 35, United States Code, § 119 of any foreign application(s) for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application on which priority is claimed:

**PRIOR FOREIGN APPLICATION(S)**

|                       |              |                         | <u>Priority Claimed</u> |
|-----------------------|--------------|-------------------------|-------------------------|
| <u>PCT/KR99/00639</u> | <u>PCT</u>   | <u>October 23, 1999</u> | Yes                     |
| (Number)              | (Country)    | (Date Filed)            |                         |
| <u>KR 1999/19192</u>  | <u>Korea</u> | <u>May 27, 1999</u>     | Yes                     |
| (Number)              | (Country)    | (Date Filed)            |                         |

I hereby claim the benefit under Title 35, United States Code, § 120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code, § 112, I acknowledge the duty to disclose all information known to me to be material to the patentability of the subject matter claimed in this application, as "materiality" is defined in Title 37, Code of Federal Regulations, § 1.56, which become available between the filing date of the prior application and the national or PCT international filing date of this application:

|                          |                |
|--------------------------|----------------|
| <u>N/A</u>               | <u>Pending</u> |
| (Application Serial No.) | (Status)       |
| <u>N/A</u>               | <u>Pending</u> |
| (Application Serial No.) | (Status)       |

PATENT  
5333-02500

I hereby claim the benefit under title 35, United States code §119(e) of any United States provisional application(s) listed below:

N/A  
(Application Serial No.) (Filing Date)

N/A  
(Application Serial No.) (Filing Date)

Please direct all communications as follows:

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I hereby declare that all statements made of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

Inventor's Full Name: Chun Byung Yang

Inventor's Signature: Chun Byung Yang Date: March 25, 2002

Country of Residence: Korea Citizenship: Korean

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